

**TECHNICAL REVIEW: STANDARD PERMIT FOR  
INSTALLATION AND/OR MODIFICATION OF OIL AND GAS FACILITIES**

<b>Permit No.:</b>	169898	<b>Company Name:</b>	Targa Pipeline Mid-Continent WestTex LLC	<b>APD Reviewer:</b>	Ms. Brittiny Williams
<b>Project No.:</b>	381386	<b>Site/Area Name:</b>	Greenwood Gas Plant	<b>SP No.:</b>	6002 - 116.620 PRE 2011-FEB-27

GENERAL INFORMATION			
<b>Regulated Entity No.:</b>	RN111549861	<b>Project Type:</b>	Standard Permit Application
<b>Customer Reference No.:</b>	CN604821355	<b>Date Received by TCEQ:</b>	October 9, 2024
<b>City/County:</b>	Midland, Midland County	<b>Date Received by Reviewer:</b>	October 10, 2024
<b>Physical Location:</b>	from intx of i-20 and sh 349 in midland, go s on sh 349 for 1 mi. go l on e county rd 120 for 11 mi. go r on fm 1379 s for 1.5 mi. site on l.		

CONTACT INFORMATION					
<b>Responsible Official/Primary Contact Name and Title:</b>	Jimmy Oxford Vice President Of Operations	<b>Phone No.:</b>	(940) 220-2493	<b>Email:</b>	JOXFORD@TARGARE SOURCES.COM
<b>Technical Contact/Consultant Name and Title:</b>	Lyndsie Slater Environmental Specialist	<b>Phone No.:</b>	(214) 420-4950	<b>Email:</b>	LSLATER@TARGARE SOURCES.COM

Compliance History Evaluation - 30 TAC Chapter 60 Rules	
A compliance history report was reviewed on:	October 11, 2024
Site rating & classification:	0.00 / High
Company rating & classification:	2.05 / Satisfactory
If site was rated unsatisfactory, what action(s) occurred as a result:	N/A

GENERAL RULES CHECK	YES	NO	COMMENTS
Is confidential information included in the application?		X	
Has the standard permit fee been paid?	X		724765 / 582EA000628594
Are there associated NSR or Title V permits at the site?	X		Title V Permit No. O4504
Is the application for renewal of an existing standard permit?		X	
Do NSPS, NESHAP, or MACT standards apply to this registration?	X		NSPS A, NSPS Dc, NSPS IIII, NSPS JJJJ, NSPS OOOOa, NSPS OOOOb, MACT A, MACT HH, MACT ZZZZ
Is the following documentation included with this registration? 1. The General Requirements Checklist demonstrating compliance with 30 TAC §§ 116.110 and 116.601-615 2. Process description 3. Project description 4. Descriptions of any equipment being installed 5. Emissions calculations including the basis of the calculations 6. Emission increases and/or decreases associated with this project (quantified) 7. Description of efforts to minimize any collateral emissions or collateral increases	X		
Are any requirements of 116.110 circumvented by: (1) artificially limiting feed or production rates below the maximum capacity of the project's equipment; (2) claiming a limited chemical list; or (3) dividing and registering a project in separate segments?		X	

STANDARD PERMIT RULES CHECK:	YES	NO	COMMENTS
Does the facility meet the § 116.14(2) definition of an Oil & Gas facility?	X		
Are there any net increases in emissions associated with this registration?	X		Please see 261/262 table below.
Does the facility vent or flare more than 0.3 long tons of sulfur (other than Sulfur Dioxide) per day?		X	
Are all emissions of sulfur compounds (other than SO2 and fugitives) controlled?		X	If NO, list the emission rate (must be ≤4 lb/hr): <del>54</del> lb/hr
Are all vents that emit sulfur compounds (other than SO2 and fugitives) to the atmosphere at least 20 feet above ground level (excluding emergency safety relief valves)?	X		List vent heights: FLR-1 = 150 ft, FLR-2 = 150 ft, FLR-PW = 20 ft, TO-1 = 57 ft, TO-2 = 57 ft
Are there new or modified internal combustion reciprocating engines or gas turbines at the facility?		X	

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Is there a natural gas glycol dehydration unit at the site that emits >10 tpy of VOCs?	X		If YES, mark the type of control device used. <u>  X  </u> flash tank _____ Vapor Recovery Unit _____ VOC destruction device _____ other															
Are any combustion units with a design maximum heat input value > 40 MBtu/hr at the site (other than flares, internal combustion engines, or natural gas turbines)?	X		If YES, list NO <sub>x</sub> emissions in pounds per MBtu.(must be < 0.06 lb/MBtu): <b>&lt; 0.06 lb/MBtu</b>															
Are VOC process fugitive emissions uncontrolled? If YES, mark applicable inspection and repair requirements. [§ 116.620(c)(1) or § 116.620(c)(2)]	X		<table border="1"> <thead> <tr> <th>VOCs (tpy)</th> <th>receptor &lt; 500'</th> <th>receptor ≥500'</th> </tr> </thead> <tbody> <tr> <td>___ &lt;10 no LDAR</td> <td>no LDAR</td> <td></td> </tr> <tr> <td>___ 10≤25 28M [(c)(1)]</td> <td>no LDAR</td> <td></td> </tr> <tr> <td>___ 25≤40 28VHP [(c)(2)]</td> <td>28M [(c)(1)]</td> <td></td> </tr> <tr> <td><u>  X  </u> &gt;40 28VHP [(c)(2)]</td> <td>28VHP [(c)(2)]</td> <td></td> </tr> </tbody> </table>	VOCs (tpy)	receptor < 500'	receptor ≥500'	___ <10 no LDAR	no LDAR		___ 10≤25 28M [(c)(1)]	no LDAR		___ 25≤40 28VHP [(c)(2)]	28M [(c)(1)]		<u>  X  </u> >40 28VHP [(c)(2)]	28VHP [(c)(2)]	
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<u>  X  </u> >40 28VHP [(c)(2)]	28VHP [(c)(2)]																	
Are all components in sweet crude oil or gas service (defined in 30 TAC Chapter 101)? If NO, mark applicable inspection and monitoring requirements. [§§ 116.620(c)(3) and 116.620(e)(1)]		X	<table border="1"> <thead> <tr> <th>RECEPTOR</th> <th>APPLICABLE REQUIREMENT</th> </tr> </thead> <tbody> <tr> <td>_____ &lt; ¼ mile</td> <td>§ 116.620(c)(3)</td> </tr> <tr> <td><u>  X  </u> ≥ ¼ mile</td> <td>§ 116.620 (c)(3) or (e)(1)</td> </tr> </tbody> </table>	RECEPTOR	APPLICABLE REQUIREMENT	_____ < ¼ mile	§ 116.620(c)(3)	<u>  X  </u> ≥ ¼ mile	§ 116.620 (c)(3) or (e)(1)									
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Are there flares at the facility?	X		The flare at the Greenwood Gas Plant will comply with the specified operational requirements.															
Is a flare the only combustion unit at the site?		X	If NO, mark the fuel type for all combustion units. <u>  X  </u> sweet natural gas _____ liquid petroleum gas _____ fuel gas ≤10 grains total sulfur/100 dscf <u>  X  </u> field gas ≤1.5 grains H <sub>2</sub> S/100 dcfm or ≤30 grains total sulfur/100 dscf _____ field gas >1.5 grains H <sub>2</sub> S/100 dcfm or >30 grains total sulfur/100 dscf (recordkeeping requirements of § 116.620(a)(18) applicable)															
Are all storage tanks onsite either (1) pressurized; (2) < 25,000 gallons in size; or (3) used for storage of compounds with vapor pressures < 0.5 psia?	X																	
Are there any fixed roof storage tanks onsite that emit > 10 tpy VOCs or sulfur compounds?		X																

DESCRIBE OVERALL PROCESS AT THE SITE

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<b>Project No.:</b>	381386	<b>Site/Area Name:</b>	Greenwood Gas Plant	<b>SP No.:</b>	6002 - 116.620 PRE 2011-FEB-27

Targa Pipeline Mid-Continent WestTex LLC (Targa) owns and operates the Greenwood Gas Plant (GP) located in Midland County, Texas.

The Greenwood Gas Plant is comprised of two trains that treat and extract natural gas liquids from natural gas. Each train will process up to 325 million standard cubic feet per day (MMSCFD) natural gas for a combined facility-wide processing capacity of 650 MMSCFD. The natural gas plant consists of inlet separation facilities, amine treating units, glycol dehydration units, cryogenic gas processing equipment, condensate stabilization, residue gas compression, nitrogen rejection units, and other supporting equipment. The supporting or auxiliary equipment for the plant consists of two hot oil heaters, two triethylene glycol (TEG) hot oil heaters, two regeneration gas heaters, electrical driven compression, two flares, two thermal oxidizers (TOs), three emergency generators, storage tanks, and pressurized condensate truck loading. A process flow diagram is included in the project file.

## **TRAIN 1**

### **Inlet, Separation, and Stabilization**

Intermediate-pressure field gas combines with the low-pressure gas from the inlet compressor and flows into the facility through the slug catchers/separators while low-pressure field gas flows into the plant and through the low-pressure slug catcher prior to entering the inlet compressors. The compressors mix the compressed inlet gas streams prior to the stabilization process. One product is made in the stabilization process: stabilized condensate. Stabilized condensate produced from the stabilization process is routed to two pressurized bullet condensate tanks (one per train). The condensate tanks are pressurized; therefore, there are no emissions from the storage tanks (EPNs: V-1409, V-1410, V-1411, and V-1412). The hot oil from the plant hot oil system (EPN: H-1701) is used to supply the heat to the stabilizer. Pressurized condensate is trucked from the facility via pressurized trucks and emissions from truck disconnects are sent to the atmosphere (EPN: PL-1).

### **Gas Treating**

After inlet separation and filtration, the inlet gas flows to a train which contains one Amine Contactor, where the gas is contacted with an aqueous solution of amine to remove carbon dioxide (CO<sub>2</sub>), hydrogen sulfide (H<sub>2</sub>S), and other incidental sulfur components. CO<sub>2</sub> and sulfur components exit from the bottom of the contactors with the rich amine which is heated and regenerated using the closed hot oil system in the amine regenerators. Hot oil is circulated and supplied by the gas-fired hot oil heater (EPN: H-1701). The vent gas is routed to the thermal oxidizer (EPN: TO-1). The acid gas is routed to the flare (EPN: FLR-1) for control during thermal oxidizer downtime. Flash vapors from the amine flash tank are routed to the low-pressure flash tank. Treated inlet gas (less CO<sub>2</sub> and sulfur components) exits the Amine Contactor and is routed to the Glycol Dehydrator.

### **Glycol Dehydrator**

A Glycol Dehydrator removes water from the gas using TEG. The TEG is then regenerated in the TEG hot oil heater. Flash gas vapors are routed to the low-pressure flash tank. Any non-condensable Benzene, Toluene, Ethylbenzene, and Xylene (BTEX) vapors from the condenser are compressed and routed to the low-pressure flash tank. This system is a closed loop; therefore, there are no emissions expected from the TEG still vent. Hot oil is circulated and supplied by the gas-fired hot oil heater (EPN: H-1703).

### **Cryogenic Gas Processing**

Gas exits the Glycol Dehydrator and flows into the Mole Sieve Dehydrator Beds. The Mole Sieve Dehydrators remove any traces of water prior to the cryogenic process. Each dehydrator contains molecular sieve dehydration beads that must be regenerated. The mole sieve beds are used to dry gas. The mole sieves are regenerated using hot gas that takes its heat from the regeneration gas heater (EPN: H-4710). The gas then goes to the cryogenic unit where gases are separated. The cooled regeneration gas is recompressed by the regeneration gas compressor to be returned to the process. After the mole sieve dehydration system, dry inlet gas goes through the dust filters and enters the cryogenic unit. In the cryogenic unit the inlet gas is cooled by cross exchanging the inlet gas with cold residue gas, cold natural gas liquids (NGLs), and propane refrigeration. As the inlet gas cools, NGLs are condensed. The NGLs are separated from the cold inlet gas in the warm and cold separators. The NGLs are discharged from the separators to the demethanizer. The cold inlet gas exiting the top of the cold separator flow through the expanders and reflux exchangers. The expanders reduce the pressure of the inlet gas and in doing so extracts work from the gas and results in condensation of additional NGLs. The two-phase mixture exiting the expanders is fed to the upper section of the demethanizers, which strips methane from the NGLs. The NGLs exit the bottom of the demethanizers with a low residual concentration of methane. The remainder of the inlet feed gas (residue gas) exits the top of the demethanizers. The cold residue gas is cross exchanged with the inlet gas to recover the refrigeration. The warm residue gas exiting the cryogenic units is compressed by electric motor driven compressors to pipeline pressure. Prior to discharge to the pipeline, the residue gas is filtered and metered. The NGL product from the cryogenic units is pumped through a sales meter and then off-site via pipeline.

### **Flare System**

There are two flares: Flare-1 (EPN FLR-1), which is used to control vapors for the amine unit during thermal oxidizer downtime and MSS operations, and a second flare (EPN: FLR-PW) that is used to control vapors from the produced water tanks and produced water loading operations from Train 1 and Train 2. The flares are designed for smokeless operation.

### **Ancillary Equipment**

The site will store various products used to maintain equipment and normal operations, including produced water, antifreeze, lube oil, used oil, contact water, amine, TEG, methanol, and anti-foam (EPNs: TK-1901 through TK-1909, TK-1911, TK-2901, TK-3901, V-4801, and TK- 9999). The produced water tanks' contents are removed from the site via atmospheric truck loading (EPN: L-1). Additional sources of emissions include fugitives from piping components (EPN FV-1), emergency engines (EPNs EG-1 and EG-3) which are authorized for 100 hours per year of testing and maintenance activities and unlimited hours for emergency use, and MSS activities. The emergency generators are authorized via PBR 106.511 claim.

## **TRAIN 2**

### **Gas Treating**

After inlet separation and filtration, the inlet gas flows to a train which contains one Amine Contactor, where the gas is contacted with an aqueous solution of amine to remove CO<sub>2</sub>, H<sub>2</sub>S, and other incidental sulfur components. CO<sub>2</sub> and sulfur components exit from the bottom of the contactors with the rich amine which is heated and regenerated using the closed hot oil system in the amine regenerators. Hot oil is circulated and supplied by the gas-fired hot oil heater (EPN: H-1704). The vent gas is routed to the thermal oxidizer (EPN: TO-2). The acid gas is routed to the flare (EPN: FLR-2) for control during thermal oxidizer downtime. Flash vapors from the amine flash tank are routed to the low-pressure flash tank. Treated inlet gas

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**DESCRIBE PROJECT AND INVOLVED PROCESS**

Targa Pipeline Mid-Continent WestTex LLC has chosen to revise and certify their site and emissions under rule 116.620 using a PI-1S.

This application makes the following changes to the existing registration:

- Updating produced water tank emissions representation
- Updating the fugitive piping components in Trains 1 and 2
- A new flare is being proposed to be installed to control emissions from produced water tanks and produced water loading operations from Trains 1 and 2.

**TECHNICAL SUMMARY - DESCRIBE HOW THE PROJECT MEETS THE RULES**

**§116.610 Applicability**

This standard permit includes all facilities at this site and conditions (a)-(d) are met.

**§116.611 Registration to Use a Standard Permit**

All required documentation has been submitted. All of conditions (a)-(c) are met.

**§116.614 Standard Permit Fees**

The \$900 fee has been submitted.

**§116.615 General Conditions**

All of general conditions (1)-(10) will be met.

**§116.620 Installation and/or Modification of Oil and Gas Facilities**

This site meets all conditions (a)-(d) of the oil and gas standard permit.

**§§106.261 / 106.262 Compliance**

The site complies with the limitations of 30 TAC §§106.261 and 106.262.

**CONTROL DEVICE(S)**

<b>Flare:</b> <b>FLR-1</b> <b>FLR-PW</b> <b>FLR-2</b>	Destruction Efficiency:	98%	Controls what?	<b>FLR-1:</b> vapors for the amine unit during thermal oxidizer downtime and MSS operations, <b>FLR-PW:</b> vapors from the produced water tanks and produced water loading operations from Train 1 and Train 2, <b>FLR-2:</b> vapors for the amine unit during thermal oxidizer downtime and MSS operations
<b>Thermal Oxidizer:</b> <b>TO-1</b> <b>TO-2</b>	Destruction Efficiency:	98%	Controls what?	<b>TO-1:</b> Vent gas from the hot oil heater (H-1701), vapors from amine unit <b>TO-2:</b> Vent gas from hot oil heater (H-1704), vapors from amine unit

**FEDERAL STANDARDS APPLICABILITY**

<i>Applicable Rule(s) :</i>	Y	NA	<i>Explanation of how it meets (if applicable), or why it isn't applicable:</i>
NSPS Subpart A	X		This subpart applies to any site that has applicable NSPS Subpart. Since Targa is subject to at least one NSPS Subpart, Targa will comply with the general requirements in Subpart A.
NSPS Subpart Dc	X		The hot oil heaters (EPN H-1701 and H-1704) and regeneration gas heaters (H-4710 and H-4711) are subject only to recordkeeping and reporting requirements, since the hot oil heater and regeneration gas heater will not burn coal, oil, or combinations of fuel that include coal and/or oil. Targa will comply with the fuel recordkeeping requirements.
NSPS Subpart IIII	X		Targa will comply with all applicable NSPS IIII requirements as they pertain to the emergency generator engines (EPNs EG-3 and EG-6) authorized via PBR 106.511.
NSPS Subpart JJJJ	X		Targa will comply with all applicable NSPS JJJJ requirements as they pertain to the emergency generator engine (EPN EG-1) authorized via PBR 106.511.
NSPS Subpart OOOOa	X		The Greenwood I Gas Plant (Train 1) was constructed after the effective date of this subpart (i.e., September 18, 2015); therefore, the following applies: The compressors are subject to NSPS OOOOa requirements. Targa will comply with all applicable requirements. The pneumatic pumps are located at

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			a natural gas processing plant and will comply with NSPS OOOOa requirements. The collection of fugitive components associated with Train 1 are subject to NSPS OOOOa for fugitive emissions. Targa will comply with the monitoring and reporting requirements for the fugitive emissions.
NSPS Subpart OOOOb	X		The Greenwood II Gas Plant (Train 2) was constructed after the effective date of this subpart, (i.e. December 6, 2022); therefore, the following applies: The compressors will be constructed after December 6, 2022; therefore, these sources will be subject to NSPS OOOOb requirements. Targa will comply with all applicable requirements. The tank battery (all 4 tanks) are uncontrolled greater than 6 tpy, so the tanks are subject to OOOOb requirements. The produced water flare (EPN: FLR-PW) is subject to NSPS OOOOb. Targa will comply with all applicable requirements. The sweetening unit is located at a natural gas processing plant and will comply with NSPS OOOOb requirements. The natural gas-driven pumps are located at a natural gas processing plant and will comply with NSPS OOOOb requirements. The non-emergency, natural gas-driven process controllers are located at a natural gas processing plant and will comply with NSPS OOOOb requirements. The collection of fugitives associated with Train 2 are subject to NSPS OOOOb for fugitive emissions. Targa will comply with the monitoring and reporting requirements for the fugitive emissions.
MACT Subpart A	X		This subpart applies to any site that has applicable MACT Subpart. Since Targa is subject to at least one MACT Subpart, Targa will comply with the general requirements in Subpart A.
MACT Subpart HH	X		This subpart applies to TEG dehydrators. The dehydrators at the Greenwood GP are only subject to the recordkeeping requirements of MACT HH since controlled benzene emissions will be less than 0.9 Megagrams per year (i.e., 1.0 tpy). Targa will maintain the proper records to comply with MACT Subpart HH.
MACT Subpart ZZZZ	X		The engines at this site were constructed after June 12, 2006; therefore, these engines, authorized via PBR 106.511, will comply with MACT ZZZZ by complying with NSPS IIII and NSPS JJJJ, as applicable.

D= 3000 and K = 8

PBR 106.261 and 106.262 Emission Limits						
Chemical	PBR Claimed	L, mg/m <sup>3</sup>	Emission Limit (E = L/K), lb/hr	Emission Limit tpy	Actual Emissions lb/hr	Actual Emissions tpy
Hydrogen Sulfide	116.620(a)(17)	10	1.250	5.00	2.76E-05	3.45E-04
Butanes	106.261(a)(2)	-	6.00	10.00	0.22	0.10
Pentanes	106.262	350	6.00	5.00	2.10	0.58
Hexanes	106.262	176	6.00	5.00	2.30	0.60
Heptane	106.262	350	6.00	5.00	0.32	0.07
Octane	106.262	350	6.00	5.00	0.06	0.01
Nonanes	106.261(a)(2)	-	6.00	10.00	0.01	1.44E-03
n-Decane	106.261(a)(3)	-	1.00	4.38	7.86E-04	1.29E-04
Benzene	106.262	3	0.375	1.6425	0.02	6.45E-04
Toluene	106.262	188	6.00	5.00	0.01	1.09E-03
Ethylbenzene	106.262	434	6.00	5.00	8.43E-04	<0.01
Xylenes	106.262	434	6.00	5.00	2.12E-03	<0.01
2,2,4-trimethylpentane	106.261(a)(3)	-	1.00	4.38	0.06	0.01
<b>Total VOC Emissions:</b>					<b>5.1037</b>	<b>1.3733</b>
<b>Total Hydrogen Sulfide Emissions</b>					<b>0.0000276</b>	<b>0.000345</b>

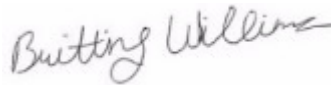

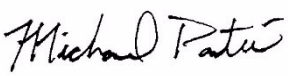
Note: Only emissions increases included in speciation.

MAXIMUM ALLOWABLE EMISSION RATES TABLE (MAERT)																	
EPN / Emission Source		VOC		NOx		CO		PM/PM10/PM2.5		SO2		H2S		CH2O		HAP	
		lbs/hr	tpy	lbs/hr	tpy	lbs/hr	tpy	lbs/hr	tpy	lbs/hr	tpy	lbs/hr	Tpy	lbs/hr	tpy	lbs/hr	Tpy
New Emissions																	
FLR- PW	PW Flare - Pilot/Assist Gas	<0.01	0.02	0.04	0.18	0.35	1.55	-	-	0.01	0.04	<0.01	<0.01	-	-	-	-
	PW Tanks Flashing/Breathing/Working	1.13	0.44	0.18	0.06	0.37	0.13	-	-	<0.01	<0.01	<0.01	<0.01	-	-	0.10	0.03
	PW Loading	2.44	0.60	0.40	0.01	0.79	0.01	-	-	<0.01	<0.01	<0.01	<0.01	-	-	0.21	0.05
Revised Emissions																	

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H-1701 / Hot Oil Heater	0.46	2.03	3.05	13.36	3.44	15.05	0.64	2.80	0.05	0.22	-	-	0.01	0.03	0.16	0.69
H-4701 / Regen Gas Heater	0.08	0.33	0.49	2.16	1.15	5.02	0.10	0.45	0.01	0.04	-	-	<0.01	<0.01	0.03	0.11
H-1703 / TEG Hot Oil Heater	0.03	0.15	0.23	0.99	0.52	2.30	0.05	0.21	<0.01	0.02	-	-	<0.01	<0.01	0.01	0.05
H-1704 / Hot Oil Heater	0.46	2.03	3.05	13.36	3.44	15.05	0.64	2.80	0.05	0.22	-	-	0.01	0.03	0.16	0.69
L-1 / Produced Water Loading	0.80	0.20	-	-	-	-	-	-	-	-	<0.01	<0.01	-	-	5.40	1.18
TK-1907 / Produced Water Tank	0.28	0.11	-	-	-	-	-	-	-	-	-	-	-	-	-	-
TK-1908 / Produced Water Tank	0.28	0.11	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FLR-1 Flare - Pilot Gas	<0.01	0.02	0.10	0.44	0.20	0.88	-	-	0.01	0.04	<0.01	<0.01	-	-	-	-
FLR-1 Flare - TO Downtime	0.61	0.06	2.78	0.28	23.83	2.38	-	-	23.23	2.32	0.24	0.02	-	-	0.17	0.02
H-4711 / Regen Gas Heater	0.08	0.33	0.49	2.16	1.15	5.02	0.10	0.45	0.01	0.04	-	-	<0.01	<0.01	0.03	0.11
H-1705 / TEG Hot Oil Heater	0.03	0.15	0.23	0.99	0.52	2.30	0.05	0.21	<0.01	0.02	-	-	<0.01	<0.01	0.01	0.05
L-2 / Produced Water Loading	0.83	0.20	-	-	-	-	-	-	-	-	<0.01	<0.01	-	-	5.40	1.18
TK-1920 / Produced Water Tank	0.28	0.11	-	-	-	-	-	-	-	-	-	-	-	-	-	-
TK-1921 / Produced Water Tank	0.28	0.11	-	-	-	-	-	-	-	-	-	-	-	-	-	-
<b>Previously Authorized Emissions</b>																
TO-1 Thermal Oxidizer	0.09	0.41	0.06	0.27	0.06	0.27	0.01	0.05	22.67	99.30	0.06	0.26	-	-	0.04	0.19
TO-1 Thermal Oxidizer - Startup	0.11	<0.01	1.96	0.01	1.65	0.01	0.15	<0.01	0.01	<0.01	-	-	-	-	-	-
FV-1 / Fugitives	5.28	23.14	-	-	-	-	-	-	-	-	0.11	0.46	-	-	0.50	2.18
PL-1 / Pressurized Loading	0.41	0.75	-	-	-	-	-	-	-	-	-	-	-	-	0.04	0.07
TK-1901 / Lube Oil Drain Sump	<0.01	<0.01	-	-	-	-	-	-	-	-	-	-	-	-	-	-
TK-1902 / Open Drain Sump	<0.01	<0.01	-	-	-	-	-	-	-	-	-	-	-	-	-	-
TK-1903 / Used Oil Tank	<0.01	<0.01	-	-	-	-	-	-	-	-	-	-	-	-	-	-
TK-1904 / New Lube Oil Tank	<0.01	<0.01	-	-	-	-	-	-	-	-	-	-	-	-	-	-
TK-1905 / Open Drain Storage Tank	<0.01	<0.01	-	-	-	-	-	-	-	-	-	-	-	-	-	-
TK-1906 / Refrigeration Lube Oil Tank	<0.01	<0.01	-	-	-	-	-	-	-	-	-	-	-	-	-	-
TK-1909 / Lean Amine Tank	<0.01	<0.01	-	-	-	-	-	-	-	-	-	-	-	-	-	-
TK-1911 / TEG Tank	<0.01	<0.01	-	-	-	-	-	-	-	-	-	-	-	-	-	-
TK-2901 / Amine Sump	<0.01	<0.01	-	-	-	-	-	-	-	-	-	-	-	-	-	-
TK-3901 / Glycol Sump	<0.01	<0.01	-	-	-	-	-	-	-	-	-	-	-	-	-	-
V-4801 / Methanol Supply Tote	1.46	0.02	-	-	-	-	-	-	-	-	-	-	-	-	1.46	0.02
TK-9999 / Anti-Foam Tote	<0.01	<0.01	-	-	-	-	-	-	-	-	-	-	-	-	-	-
TO-2 Thermal Oxidizer	1.84	8.04	0.06	0.27	0.06	0.28	0.01	0.05	23.07	101.04	0.06	0.27	-	-	0.15	0.67
TO-2 Thermal Oxidizer - Startup	0.11	<0.01	1.96	0.01	1.65	0.01	0.15	<0.01	0.01	<0.01	-	-	-	-	-	-
FLR-2 Flare - Pilot Gas	<0.01	0.02	0.10	0.44	0.20	0.88	-	-	0.01	0.04	<0.01	<0.01	-	-	-	-
FLR-2 Flare - TO Downtime	7.45	0.75	2.78	0.28	23.83	2.38	-	-	23.63	2.36	0.25	0.02	-	-	0.61	0.06
NRU-2 / Nitrogen Rejection Unit	<0.01	<0.01	-	-	-	-	-	-	-	-	-	-	-	-	-	-
FV-2 / Fugitives	4.62	20.24	-	-	-	-	-	-	-	-	<0.01	<0.01	-	-	0.32	1.40
<b>TOTAL EMISSIONS (TPY):</b>		<b>60.37</b>		<b>35.27</b>		<b>53.52</b>		<b>7.02</b>		<b>205.70</b>		<b>1.03</b>		<b>0.06</b>		<b>8.75</b>
<b>MAXIMUM OPERATING SCHEDULE: Hours/Year</b>																<b>8760</b>

	TECHNICAL REVIEWER	PEER REVIEWER	FINAL REVIEWER
<b>SIGNATURE:</b>			
<b>PRINTED NAME:</b>	Ms. Brittiny Williams, Reviewer	Trishia McDonald, Team Leader	Michael Partee, Manager
<b>DATE:</b>	11/08/2024	11/08/2024	11/08/2024