

Pioneer Natural Resources USA, Inc. 3617 N. Big Spring St. Midland, Texas 79705 Main: (432) 571-1000

May 27, 2021

Mr. Ryan Slocum Region 7 Section Manager Texas Commission on Environmental Quality 9900 West IH-20, Suite 100 Midland, Texas 79706

RE: 40 CFR 60 Subpart JJJJ, Post-test Notification of Compliance Status

Scharbauer Ranch 323-14H Tank Battery ENG 2 GPS Coordinates: 32.273019, -102.143394

Customer Number: CN600130447 Regulated Entity No.: 107031288

PBR No.: 115606

Dear Mr. Slocum:

Pioneer Natural Resources USA, Inc., pursuant to 40 CFR §60.8(a) and 40 CFR §60.4245(d), is submitting this Notification of Compliance Status no later than sixty (60) days after completion of an engine performance test conducted on May 19, 2021 for the engine below located at the Scharbauer Ranch 323-14H Battery in Martin County, Texas.

Unit No.	Make	Model	Serial No.	Mfg. HP@RPM
Kodiak Unit #16-0436	Caterpillar	3516B LE	JEF03385	1380 @ 1400
Displacement	Engine Emissions	Overhaul Date	Fuel Used	Engine Family
1	Control			,
69.0 L	Oxidation Catalyst	4-29-2019	Natural Gas	SI 4SLB

If you have any questions, please contact me at 432-254-1347 o

Best Regards,

Efrain Vizcaino

Engine Compliance Tech. III

cc: Shyla Harris, Environmental Compliance Manager, Pioneer Natural Resources USA, Inc.

Enclosure: JJJJ Performance Test Report

40 CFR Part 60 Subpart JJJJ
Performance Test Report

Test Type: Annual
Test Date: 05-19-2021
DOM: 04-29-19
Source:
Caterpillar 3516B LE
Lean Burn 4 Cycle Engine

Unit Number: ENG 2 (K16-0436) Serial Number: JEF03385 Engine Hours: 17348 CN #: 600130447 RN #: 107031288

Permit #: #PBR 115606

Location: Scharbauer Ranch 323-14H Tank Battery Martin County, Texas

Prepared on Behalf of:Pioneer Natural Resources

<i>mananana</i>	CC)		NOx		NIN	ΛΝΕΗC (V)()	W		W			XX	XXX	XXX
	Federal Sta	100000000	Federal	State	<i>illillilli</i>	Federal	State	<u>Millilli</u>		\mathcal{H}	W		\mathcal{H}	1		XX
Results ppmvd	30.4			102.220	NANANA		21.208	17777777		\mathcal{H}			\mathcal{H}			$\widetilde{\mathcal{U}}$
											\overline{M}				\overline{W}	$\overline{\mathcal{M}}$
	mmm															
									\overline{M}		\overline{m}				\overline{Z}	\overline{Z}
	<u> </u>	<u> </u>	71111111		W/////				$\langle \rangle \rangle$	<i>333</i>	\overline{m}	777	<i>333</i>	M	\widetilde{m}	\overleftrightarrow{m}
Results g/hp-hr	0.1	le reconstructeres		0.554	<u> </u>		0.110	<u> </u>							<u> </u>	
Permit g/hp-hr	2.000 2.0	00	1.000	1.000		0.700	0.400				\mathscr{W}	777		$\frac{1}{2}$	$\stackrel{22}{44}$	$\widetilde{\mathcal{W}}$
								<u> </u>		9			9		<i></i>	$\frac{20}{20}$
PASS ALL	Pass Pa		Pass	Pass		Pass	Pass			<u> </u>			<u> </u>			\mathcal{H}

Test Started: 6:28 Test Completed: 9:48



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1.0 Key Personnel

Great Plains Analytical Services Pioneer

Cory Garrison Efrain Vizcaino

2.0 Sampling System

The sampling system used consisted of a Stainless steel probe, heated Teflon line, gas conditioning system, and a Gasmet model DX4000 FTIR analyzer. The gas conditioning system used was a Gasmet Personal Sampling System with a Zirconium Oxide oxygen sensor.

3.0 Methods Used

ASTM D6348-03

This extractive FTIR based field test method is used to quantify gas phase concentrations of multiple target analytes (CO, NOX, CH2O, & VOC's) from stationary source effluent. Because an FTIR analyzer is potentially capable of analyzing hundreds of compounds, this test method is not analyte or source specific. The analytes, detection levels, and data quality objectives are expected to change for any particular testing situation. It is the responsibility of the tester to define the target analytes, the associated detection limits for those analytes in the particular source effluent, and the required data quality objectives for each specific test program. Provisions are included in this test method that require the tester to determine critical sampling system and instrument operational parameters, and for the conduct of QA/QC procedures. Testers following this test method will generate data that will allow an independent observer to verify the valid collection, identification, and quantification of the subject target analytes.

EPA Method 1

The purpose of the method is to provide guidance for the selection of sampling ports and traverse points at which sampling for air pollutants will be performed pursuant to regulations set forth in this part.

EPA Method 2 & 2C

This method is applicable for the determination of the average velocity and the volumetric flow rate of a gas stream. The average gas velocity in a stack is determined from the gas density and from measurement of the average velocity head with a standard pitot tube. Velocity readings are taken from each stack at 16 separate traverse points (Table 6.1) and used to determine the engines mass emissions rate, calculated utilizing the formulas seen in section 7.0 of this report.

EPA Method 3A

This is a procedure for measuring oxygen (O2) and carbon dioxide (CO2) in stationary source emissions using a continuous instrumental analyzer. Quality assurance and quality control requirements are included to assure that the tester collects data of known quality. Documentation to these specific requirements for equipment, supplies, sample collection and analysis, calculations, and data analysis will be included.

4.0 Test Summary

Unit ENG 2 (K16-0436) with a serial number of JEF03385 which is a Caterpillar 3516B LE engine located at Scharbauer Ranch 323-14H Tank Battery and operated by Pioneer Natural Resources was tested for emissions of: (Oxides of Nitrogen) (Carbon Monoxide) (Volatile Organic Compounds). The test was conducted on 05-19-2021 by Cory Garrison with Great Plains Analytical Services, Inc. All quality assurance and quality control tests were within acceptable tolerances.

The engine is a natural gas fired Lean Burn (4 Cycle) engine rated at 1380 brake horse power (BHP) at 1400 RPM. The engine was operating at 1328.04 BHP and 1300 RPM which is 96.23% of maximum engine load during the test. The test HP calculation can be found on page 8. The engine was running at the maximum load available at the test site.

This test will satisfy the testing requirements for 40 CFR Part 60 Subpart JJJJ. Unit ENG 2 (K16-0436) is authorized to operate under permit #PBR 115606.

Site Verification Photos



4.0 Test Summary

						io rest summary
						ngine/Compressor Specs
) T	ENG 2 (K16-0436)	Unit ID		anch 323-14H	Location Scharbauer I	Location
"	2884	Site Elevation ft.			Make Caterpillar	Maki
е	13.23	heric Pressure psi.	Atmosp		Model 3516B LE	Mode
	15.75	Stack Diameter in.			Serial number JEF03385	Serial numbe
S	Yes	Catalyst			mfg. rated hp 1380	mfg. rated h
	4/29/19	Date of Manufacture			mfg. rated rpm 1400	mfg. rated rpn
t	3 Run Average	Run 3	Run 2	Run 1		ngine/Compressor Operation
	1328	1328	1327	1328	Test Horsepower	Tes
	1300	1300	1299	1300	Test RPM	
S	96.23%	96.26%	96.19%	96.26%	Percent Load %	Pe
3	64.68	64.68	64.68	64.68	ntake Manifold Pressure (hg)	Intake Manifold
и	137.33	138.00	137.00	137.00	ke Manifold Temperature (F)	Intake Manifold Ter
u						mbient Conditions
m	63.00	62.00	63.00	64.00	Ambient Temperature Dry (F)	Ambient Tempe
						khaust Flow Data
m	132960.47	142801.65	133051.65	123028.09	Q Stack (dscfh)	Q
	3764.99	4043.65	3767.57	3483.73	Q Stack (dscm/hr)	Q Sto
а	0.12	0.12	0.12	0.12	Moisture Fraction Bws	Moisture
r						
у						
		ılts	Resu			
	9.10%	9.12%	9.07%	9.11%	od 3A Corrected O2% Dry	Method 3A Correct
	12.18%	12.20%	12.49%	11.84%	Moisture %	

	Perm	itted Stand	dards		Results					
	Test Sta	rt/Comple	ted Times:	6:28	7:35	8:41	9:48	5/19/21		
	וווו	State		Run 1	Run 2	Run 3	3 Run Average	Pass Permits		
CO (g/hp-hr)	2.000	2.000		0.097	0.097	0.107	0.100	Pass		
CO (ppmvd) @15% O2				15.887	14.714	15.063	15.221			
CO (ppbvd) @15% O2				15886.509	14714.452	15063.134	15221.365			
CO (ppmvw)				27.985	25.815	26.395	26.732			
CO (ppmvd)				31.743	29.498	30.063	30.435			
			CO (mol wt)	28.01						
NOx (g/hp-hr)	1.000	1.000		0.510	0.567	0.585	0.554	Pass		
NOx (ppmvd) @15% O2				50.887	52.098	50.377	51.120			
NOx (ppbvd) @15% O2	////////			50886.784	52097.654	50376.897	51120.445			
NOx (ppmvw)				89.640	91.400	88.275	89.772			
NOx (ppmvd)				101.679	104.439	100.541	102.220			
	•	N	Ox (mol wt)	46.01				•		
NMNEHC (g/hp-hr)	0.700	0.400		0.101	0.114	0.116	0.110	Pass		
NMNEHC (ppmvd) @15% O2				10.502	10.913	10.404	10.606			
NMNEHC (ppbvd) @15% O2				10502.069	10912.578	10403.521	10606.056			
NMNEHC (ppmvw)				18.500	19.145	18.230	18.625			
NMNEHC (ppmvd)				20.985	21.876	20.763	21.208			
		V	OC (mol wt)	44.10						

5.0 Run Summaries

Table 5.1 Run Summaries

ımmary Source l	Run 1						
PPM Wet	СО	NO	NO2	NOx	NMNEHC	Oxygen %	Moisture %
Baseline	0.00	0.00	0.00	0.00	0.00	0.00%	0.00%
Source	29.61	77.06	11.96	89.02	18.88	7.88%	11.62%
Spike	60.13	89.31	6.52	95.83	37.00	7.38%	10.97%
Source	26.36	74.87	15.39	90.26	18.12	7.74%	12.06%
Baseline	1.22	0.00	0.11	0.11	1.75	0.00%	0.00%
Avg. Wet	27.99	75.97	13.68	89.64	18.50	7.81%	11.84%
ımary Source I	Run 2						
PPM Wet	СО	NO	NO2	NOx	NMNEHC	Oxygen %	Moisture %
Baseline	1.22	0.00	0.11	0.11	1.75	0.00%	0.00%
Source	26.09	75.59	17.94	93.53	18.96	7.82%	12.27%
Spike	57.69	87.49	9.80	97.29	37.44	7.25%	11.56%
Source	25.54	73.53	15.74	89.27	19.33	7.62%	12.70%
Baseline	1.17	0.00	0.03	0.03	1.62	0.00%	0.00%
Avg. Wet	25.82	74.56	16.84	91.40	19.15	7.72%	12.49%
ımary Source I	Run 3						
PPM Wet	СО	NO	NO2	NOx	NMNEHC	Oxygen %	Moisture %
Baseline	1.17	0.00	0.03	0.03	1.62	0.00%	0.00%
Source	26.14	75.64	12.42	88.06	19.44	7.83%	12.32%
Spike	58.36	90.24	7.08	97.32	36.92	7.37%	11.34%
Source	26.65	78.35	10.14	88.49	17.02	7.75%	12.08%
Baseline	1.11	0.00	0.28	0.28	1.43	0.00%	0.00%
Avg. Wet	26.40	77.00	11.28	88.28	18.23	7.79%	12.20%

6.0 Volumetric Flow Rate Data

Table 6.1. Data used for volumetric flow rate (Method 2)

	Volumetric	flow rate data				V
Pitot Tube Coefficient Cp(std)= 0.99						•
Stack diameter = 15.75	inches or:	1.31	feet or:	1.35	Square Feet	0
		Run 1	Run 2	Run 3	Average	I
H2O	%d	11.84	12.49	12.20	12.18	u
CO2	%d	5.76	5.76	5.73	5.75	m
02	%d	7.81	7.72	7.79	7.77	
CO	ppmd	27.99	25.82	26.40	26.73	е
Molecular Weight Stack Gas dry basis (Md)	g/g mole	29.23	29.23	29.23	29.23	t
Molecular Weight Stack Gas wet basis (Ms)	g/g mole	27.90	27.83	27.86	27.86	r
Stack Static Pressure (Pg)	"H20	0.41	0.49	0.56	0.49	i
Stack Static Pressure (Pg)	"Hg	0.03	0.04	0.04	0.04	,
Atmospheric Pressure at Location (Pbar)	MBAR	910.72	911.15	912.53	911.46	С
Atmospheric Pressure at Location (Pbar)	"Hg	26.90	26.91	26.95	26.92	
Absolute Stack Pressure (Ps)	"Hg	26.93	26.95	26.99	26.96	F
Stack Temperature	Deg C	327.85	328.85	332.60	329.77	,
Stack Temperature	Deg F	622.13	623.94	630.69	625.58	
Stack Temperature	Deg R	1081.80	1083.61	1090.36	1085.25	0
Stack Gas Velocity	ft/sec	65.22	71.13	76.43	71.06	w
Stack Flow Rate Q	cfs	88.24	96.23	103.41	96.14	
Stack Gas Wet Volmetric Flow Rate	scf/hr	139550.92	152032.97	162644.25	151717.53	
Stack Gas Dry Volumetric Flow Rate	scf/hr	123028.09	133051.65	142801.65	133245.93	R
						а
		Emissions Samplin	Inches	t		
	7% of Stack Diameter	2.63	е			
		Second Samp	oling Point Taken @ 5	0% of Stack Diameter	7.88	
		Third Sampli	ng Point Taken @ 83.	3% of Stack Diameter	13.12	S

Table 6.2. Stack gas pressure readings measured with a standard pitot tube used for Volumetric Flow

nate						
Δp_{std} = Velocity head measured by the standard pitot	Ru	ın 1	Ru	n 2	Ru	ın 3
tube, cm (in.) H2O.	Δpstd in H2O	Exhaust Temp F	Δpstd in H2O	Exhaust Temp F	Δpstd in H2O	Exhaust Temp F
Pitot Tube Sampling Points (Velocity)						
1	0.420	622.00	0.420	624.00	0.410	631.00
2	0.490	621.00	0.420	622.00	0.480	630.00
3	0.470	623.00	0.470	621.00	0.570	628.00
4	0.450	620.00	0.530	622.00	0.580	624.00
5	0.460	624.00	0.570	624.00	0.590	633.00
6	0.370	627.00	0.530	626.00	0.550	630.00
7	0.400	625.00	0.560	625.00	0.600	634.00
8	0.350	622.00	0.510	620.00	0.570	632.00
9	0.300	620.00	0.550	622.00	0.550	633.00
10	0.450	620.00	0.470	627.00	0.560	629.00
11	0.490	619.00	0.430	629.00	0.590	627.00
12	0.490	617.00	0.430	628.00	0.610	628.00
13	0.530	622.00	0.550	627.00	0.520	631.00
14	0.320	624.00	0.490	622.00	0.620	633.00
15	0.300	625.00	0.470	624.00	0.580	635.00
16	0.310	623.00	0.420	620.00	0.620	633.00
ostd Average=	0.413	622.13	0.489	623.94	0.563	630.69

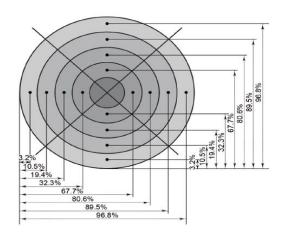
Sample after Back Purge:	0.62
Within 5% of last Δpstd reading:	Yes
Stack Diameter (inches)	15.75

Stack Diameter (inches)	15.75
Inches upstream from disturbance	8.00
Inches downstream from disturbance	40.00

Pitot readings are taken for Method 2 calculations using measuring points outlined in Method 1

Figure 6.1

16 Traverse Points Were Used



Mathad 2: Data	7.0 Calculations
	ination of Stack Gas Velocity and Volumetric Flow Rate tes the need for any fuel related numbers for emissions calculations
note ose of this method nega	Nomenclature
Δp(avg) = Velocity head of stack gas, mm H2O (in. H2O).	Ps = Absolute stack pressure (Pbar+ Pg), mm Hg
3600 = Conversion Factor, sec/hr. A = Cross-sectional area of stack, m2 (ft2).	(in Hg) Pstd = Standard absolute pressure, 760 mm Hg
Bws = Water vapor in the gas stream (from ASTM	(29.92 in. Hg).
D6348)	Qsd = Dry volumetric stack gas flow rate corrected
Cp(std) = Standard pitot tube coefficient; use 0.99	to standard conditions, dscm/hr. (dscf/hr.).
Kp = Velocity equation constant.	Ts(abs) = Absolute stack temperature, °K (°R).
Md = Molecular weight of stack gas, dry basis, g/g-mole	= 460 + Ts for English units.
(lb./lbmole).	Tstd = Standard absolute temperature,
Ms = Molecular weight of stack gas, wet basis, g/g-mole (lb./lbmole).	293°K (528°R). Vs = Average stack gas velocity, m/sec (ft./sec).
	Method 3 12.3) Dry Molecular Weight. Equation 3-1
(0000.1764.1761.1	method 5 12.5/5/7 morecard metgrat 24ddaton 5 1
Md=.44(%CO2)+.32(%O2)+.28(%N2+%CO)	Md=.44(0.058)+.32(0.091)+.28(0.848+0.003) =29.234LB/LB-MOLE
Vicinity of the control of the contr	(,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,
12.5 M	lolecular Weight of Stack Gas. Equation 2-6
12.5 (Meight of Stack Oas. Equation 2 o
Ms=Md(1-Bws)+18.0(Bws)	Ms=29.234(1-0.118)+18.0(0.118) =27.904LB/LB-MOLE
1815-1810(1 BW3):10.0(BW3)	MS-23.234(1 0.110).10.0(0.110) -27.304E0/E0 MOEE
12.6	Average Stack Gas Velocity. Equation 2-7
	- The age stack our velocity. Equation 2.7-
Vs=Kp*Cp(std)*v∆pavg*v(Ts(abs)/(Ps*Ms))	Vs=85.49*0.99*v0.413*v(1081.795/(26.929*27.904)) =65.221FT/SEC
A3-Wh Chistol Athank A(12(an2)/(L2 IAI2))	v3-03.43 0.33 v0.413 v[1001./23]/(20.323 2/.304]) =03.221F1/3EC
427.	
12./ Averag	e Stack Gas Volumetric Flow Rate. Equation 2-8
Qsd=3600(1-Bws)Vs*A{(Tstd*Ps)/(Ts(abs)*Pstd)}	Qsd=3600(1-0.118)65.221*1.353{(528*26.929)/ (1081.795*29.92)} =123028.093DSCF/HR
*0	andard conversion from feet to meters
.3	andard conversion from feet to meters
Q=Qsd/35.315	Q=123028.093/35.315 =3483.735 DSCM/HR
ζ-ωμ/55.515	Q=123028.053/35.313 =3463.733 b3C(V)/11K
E	nission Rates (Examples use CO Run 1)
	Nomenclature
453.6= Conversion factor lb. to gram	HP= Engines rated Horsepower
A = Cross-sectional area of stack, m2 (ft2).	Mfg.= Manufacturer Exhaust flow rate at 100%
BHP/HR. = Brake work of the engine, horsepower-hour (HP-HR.).	(ft3/min) O2 = Concentration of oxygen on a dry basis,
BTU/HP-HR. = Brake Specific Fuel Consumption (HHV)	percent.
ER = Emission rate of (CO) in g/HP-hr.	ppm= Parts Per Million (CO)
F(d)= Volumes of combustion components per unit of heat	ppm@15% O2=PPM corrected to 15% O2
content, scm/J (scf/million Btu).	Qsd = Dry volumetric stack gas flow rate corrected
Q = Stack gas volumetric flow rate, in standard cubic meters	
per hour, dry basis	to standard conditions, dscm/hr. (DSCF/HR.).
ILB/HR = Emission rate of (CO) in LB/HR	Run Time = Run Time in Minutes
LB/HR.= Emission rate of (CO) in LB/HR. Mol wt.= Mol Weight of CO (28.01)	
* * * *	Run Time = Run Time in Minutes TPY= Tons per Year
, , ,	Run Time = Run Time in Minutes TPY= Tons per Year Vs = Average stack gas velocity, m/sec (ft./sec).
* * * *	Run Time = Run Time in Minutes TPY= Tons per Year Vs = Average stack gas velocity, m/sec (ft./sec).
Mol wt.=Mol Weight of CO (28.01)	Run Time = Run Time in Minutes TPY= Tons per Year Vs = Average stack gas velocity, m/sec (ft./sec). CO corrected @ 15% O2
Mol wt.= Mol Weight of CO (28.01) ppm @ 15% O2=PPM*{(20.9-15%O2)/(20.9-O2)}	Run Time = Run Time in Minutes TPY= Tons per Year Vs = Average stack gas velocity, m/sec (ft./sec). CO corrected @ 15% O2
Mol wt.= Mol Weight of CO (28.01) ppm @ 15% O2=PPM*{(20.9-15%O2)/(20.9-O2)}	Run Time = Run Time in Minutes TPY= Tons per Year Vs = Average stack gas velocity, m/sec (ft./sec). CO corrected @ 15% O2 ppm @ 15% O2=31.743*{(20.9-15)/(20.9-9.10%)}=15.887 PPM@ 15% O2
Mol wt.= Mol Weight of CO (28.01) ppm @ 15% O2=PPM*{(20.9-15%O2)/(20.9-O2)}	Run Time = Run Time in Minutes TPY= Tons per Year Vs = Average stack gas velocity, m/sec (ft./sec). CO corrected @ 15% O2 ppm @ 15% O2=31.743*{(20.9-15)/(20.9-9.10%)}=15.887 PPM@ 15% O2
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Mol wt.= Mol Weight of CO (28.01) ppm @ 15% O2=PPM*{(20.9-15%O2)/(20.9-O2)}	Run Time = Run Time in Minutes TPY= Tons per Year Vs = Average stack gas velocity, m/sec (ft./sec). CO corrected @ 15% O2 ppm @ 15% O2=31.743*{(20.9-15)/(20.9-9.10%)}=15.887 PPM@ 15% O2 HP HR From 40 CFR Part 60 Subpart JJJJ
Mol wt.= Mol Weight of CO (28.01) ppm @ 15% O2=PPM*{(20.9-15%O2)/(20.9-O2)}	Run Time = Run Time in Minutes TPY= Tons per Year Vs = Average stack gas velocity, m/sec (ft./sec). CO corrected @ 15% O2 ppm @ 15% O2=31.743*{(20.9-15)/(20.9-9.10%)}=15.887 PPM@ 15% O2 HP HR From 40 CFR Part 60 Subpart JJJJ (31.743*(1.164*10^3)*3483.735*(Run Time/60))/1328.382 = 0.097 G/HP-HR
Mol wt.= Mol Weight of CO (28.01) ppm @ 15% O2=PPM*{(20.9-15%O2)/(20.9-O2)}	Run Time = Run Time in Minutes TPY= Tons per Year Vs = Average stack gas velocity, m/sec (ft./sec). CO corrected @ 15% O2 ppm @ 15% O2=31.743*{(20.9-15)/(20.9-9.10%)}=15.887 PPM@ 15% O2 HP HR From 40 CFR Part 60 Subpart JJJJ (31.743*(1.164*10^3)*3483.735*(Run Time/60))/1328.382 = 0.097 G/HP-HR
Mol wt.= Mol Weight of CO (28.01) ppm @ 15% O2=PPM*{(20.9-15%O2)/(20.9-O2)} G/l g/hp-hr={PPM*(1.164*10^-3)*Q*{Run Time/60)}/BHP/HR	Run Time = Run Time in Minutes TPY= Tons per Year Vs = Average stack gas velocity, m/sec (ft./sec). CO corrected @ 15% O2 ppm @ 15% O2=31.743*{(20.9-15)/(20.9-9.10%)}=15.887 PPM@ 15% O2 HP HR From 40 CFR Part 60 Subpart JJJJ (31.743*(1.164*10^-3)*3483.735*(Run Time/60))/1328.382 = 0.097 G/HP-HR LB/HR from Grams
Mol wt.= Mol Weight of CO (28.01) ppm @ 15% O2=PPM*{(20.9-15%O2)/(20.9-O2)} G/l g/hp-hr={PPM*(1.164*10^-3)*Q*(Run Time/60))/BHP/HR	Run Time = Run Time in Minutes TPY= Tons per Year Vs = Average stack gas velocity, m/sec (ft./sec). CO corrected @ 15% O2 ppm @ 15% O2=31.743*{(20.9-15)/(20.9-9.10%)}=15.887 PPM@ 15% O2 HP HR From 40 CFR Part 60 Subpart JJJJ (31.743*(1.164*10^-3)*3483.735*(Run Time/60))/1328.382 = 0.097 G/HP-HR LB/HR from Grams
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Mol wt.= Mol Weight of CO (28.01) ppm @ 15% O2=PPM*{(20.9-15%O2)/(20.9-O2)} G/l g/hp-hr={PPM*(1.164*10^-3)*Q*(Run Time/60))/BHP/HR	Run Time = Run Time in Minutes TPY= Tons per Year Vs = Average stack gas velocity, m/sec (ft./sec). CO corrected @ 15% O2 ppm @ 15% O2=31.743*{(20.9-15)/(20.9-9.10%)}=15.887 PPM@ 15% O2 HP HR From 40 CFR Part 60 Subpart JJJJ (31.743*(1.164*10^-3)*3483.735*(Run Time/60))/1328.382 = 0.097 G/HP-HR LB/HR from Grams LB/HR=0.097*1/453.6*1328.382=0.284
Mol wt.= Mol Weight of CO (28.01) ppm @ 15% O2=PPM*{{20.9-15%O2}/{20.9-02}} G/l g/hp-hr={PPM*(1.164*10^-3)*Q*(Run Time/60)}/BHP/HR Ib/hr=ER*1/453.6*BHP-HR	Run Time = Run Time in Minutes TPY= Tons per Year Vs = Average stack gas velocity, m/sec (ft./sec). CO corrected @ 15% O2 ppm @ 15% O2=31.743*{(20.9-15)/(20.9-9.10%)}=15.887 PPM@ 15% O2 HP HR From 40 CFR Part 60 Subpart JJJJ (31.743*(1.164*10^-3)*3483.735*(Run Time/60))/1328.382 = 0.097 G/HP-HR LB/HR from Grams LB/HR=0.097*1/453.6*1328.382=0.284
Mol wt.= Mol Weight of CO (28.01) ppm @ 15% O2=PPM*{{20.9-15%O2}/{20.9-02}} G/l g/hp-hr={PPM*(1.164*10^-3)*Q*(Run Time/60)}/BHP/HR Ib/hr=ER*1/453.6*BHP-HR	Run Time = Run Time in Minutes TPY= Tons per Year Vs = Average stack gas velocity, m/sec (ft./sec). CO corrected @ 15% O2 ppm @ 15% O2=31.743*{(20.9-15)/(20.9-9.10%)}=15.887 PPM@ 15% O2 HP HR From 40 CFR Part 60 Subpart JJJJ (31.743*(1.164*10^-3)*3483.735*(Run Time/60))/1328.382 = 0.097 G/HP-HR LB/HR from Grams LB/HR=0.097*1/453.6*1328.382=0.284
Mol wt.= Mol Weight of CO (28.01) ppm @ 15% O2=PPM*{(20.9-15%O2)/(20.9-O2)} G/ g/hp-hr=(PPM*(1.164*10^-3)*Q*(Run Time/60))/BHP/HR Ib/hr=ER*1/453.6*BHP-HR TPY=LB/HR. *4.38	Run Time = Run Time in Minutes TPY= Tons per Year Vs = Average stack gas velocity, m/sec (ft./sec). CO corrected @ 15% O2 ppm @ 15% O2=31.743*{(20.9-15)/(20.9-9.10%)}=15.887 PPM@ 15% O2 HP HR From 40 CFR Part 60 Subpart JJJJ (31.743*(1.164*10^-3)*3483.735*(Run Time/60))/1328.382 = 0.097 G/HP-HR LB/HR from Grams LB/HR=0.097*1/453.6*1328.382=0.284 TPY TPY=0.3*4.38 = 1.243 TPY
Mol wt.= Mol Weight of CO (28.01) ppm @ 15% O2=PPM*{{20.9-15%O2}/{20.9-O2}} g/hp-hr={PPM*(1.164*10^-3)*Q*(Run Time/60)}/BHP/HR Ib/hr=ER*1/453.6*BHP-HR TPY=LB/HR. *4.38 BHP/HR = Available HP - ((MFP @100% - Actual MFP inHG) /	Run Time = Run Time in Minutes TPY= Tons per Year Vs = Average stack gas velocity, m/sec (ft./sec). CO corrected @ 15% O2 ppm @ 15% O2=31.743*{(20.9-15)/(20.9-9.10%)}=15.887 PPM@ 15% O2 HP HR From 40 CFR Part 60 Subpart JJJJ (31.743*(1.164*10^-3)*3483.735*(Run Time/60))/1328.382 = 0.097 G/HP-HR LB/HR from Grams LB/HR=0.097*1/453.6*1328.382=0.284 TPY TPY=0.3*4.38 = 1.243 TPY
Mol wt.= Mol Weight of CO (28.01) ppm @ 15% O2=PPM*{(20.9-15%O2)/(20.9-02)} G/ g/hp-hr=(PPM*(1.164*10^-3)*Q*(Run Time/60))/BHP/HR Ib/hr=ER*1/453.6*BHP-HR TPY=LB/HR. *4.38	Run Time = Run Time in Minutes TPY= Tons per Year Vs = Average stack gas velocity, m/sec (ft./sec). CO corrected @ 15% O2 ppm @ 15% O2=31.743*((20.9-15)/(20.9-9.10%))}=15.887 PPM@ 15% O2 HP HR From 40 CFR Part 60 Subpart JJJJ (31.743*(1.164*10^-3)*3483.735*(Run Time/60))/1328.382 = 0.097 G/HP-HR LB/HR from Grams LB/HR=0.097*1/453.6*1328.382=0.284 TPY TPY=0.3*4.38 = 1.243 TPY
Mol wt.= Mol Weight of CO (28.01) ppm @ 15% O2=PPM*{{20.9-15%O2}/{20.9-O2}} g/hp-hr=(PPM*(1.164*10^-3)*Q*(Run Time/60))/BHP/HR lb/hr=ER*1/453.6*BHP-HR TPY=LB/HR. *4.38 BHP/HR = Available HP - ((MFP @100% - Actual MFP inHG) /	Run Time = Run Time in Minutes TPY= Tons per Year Vs = Average stack gas velocity, m/sec (ft./sec). CO corrected @ 15% O2 ppm @ 15% O2=31.743*{(20.9-15)/(20.9-9.10%)}=15.887 PPM@ 15% O2 HP HR From 40 CFR Part 60 Subpart JJJJ (31.743*(1.164*10^-3)*3483.735*(Run Time/60))/1328.382 = 0.097 G/HP-HR LB/HR from Grams LB/HR=0.097*1/453.6*1328.382=0.284 TPY TPY=0.3*4.38 = 1.243 TPY Horsepower 1328 = 1281.42857142857 - ((89.1 - 92) / ((89.1 - 71.9) / 25%))) * 1281.42857142857
Mol wt.= Mol Weight of CO (28.01) ppm @ 15% O2=PPM*{{20.9-15%O2}/{20.9-O2}} g/hp-hr=(PPM*(1.164*10^-3)*Q*(Run Time/60))/BHP/HR lb/hr=ER*1/453.6*BHP-HR TPY=LB/HR. *4.38 BHP/HR = Available HP - ((MFP @100% - Actual MFP inHG) /	Run Time = Run Time in Minutes TPY= Tons per Year Vs = Average stack gas velocity, m/sec (ft./sec). CO corrected @ 15% O2 ppm @ 15% O2=31.743*((20.9-15)/(20.9-9.10%))}=15.887 PPM@ 15% O2 HP HR From 40 CFR Part 60 Subpart JJJJ (31.743*(1.164*10^-3)*3483.735*(Run Time/60))/1328.382 = 0.097 G/HP-HR LB/HR from Grams LB/HR=0.097*1/453.6*1328.382=0.284 TPY TPY=0.3*4.38 = 1.243 TPY
Mol wt.= Mol Weight of CO (28.01) ppm @ 15% O2=PPM*{(20.9-15%O2)/(20.9-O2)} G/I g/hp-hr=(PPM*(1.164*10^-3)*Q*(Run Time/60))/BHP/HR Ib/hr=ER*1/453.6*BHP-HR TPY=LB/HR. *4.38 BHP/HR = Available HP - ((MFP @100% - Actual MFP inHG) / ((MFP @100% - MFP @75%) / 25%))) * Available HP	Run Time = Run Time in Minutes TPY= Tons per Year Vs = Average stack gas velocity, m/sec (ft./sec). CO corrected @ 15% O2 ppm @ 15% O2=31.743*((20.9-15)/(20.9-9.10%)) = 15.887 PPM@ 15% O2 IP HR From 40 CFR Part 60 Subpart JJJJ (31.743*(1.164*10^-3)*3483.735*(Run Time/60))/1328.382 = 0.097 G/HP-HR LB/HR from Grams LB/HR=0.097*1/453.6*1328.382=0.284 TPY TPY=0.3*4.38 = 1.243 TPY Horsepower 1328 = 1281.42857142857 - ((89.1 - 92) / ((89.1 - 71.9) / 25%))) * 1281.42857142857 Wet to Dry PPM
Mol wt.= Mol Weight of CO (28.01) ppm @ 15% O2=PPM*{{20.9-15%O2}/{20.9-O2}} g/hp-hr={PPM*(1.164*10^-3)*Q*(Run Time/60)}/BHP/HR Ib/hr=ER*1/453.6*BHP-HR TPY=LB/HR. *4.38 BHP/HR = Available HP - ((MFP @100% - Actual MFP inHG) /	Run Time = Run Time in Minutes TPY= Tons per Year Vs = Average stack gas velocity, m/sec (ft./sec). CO corrected @ 15% O2 ppm @ 15% O2=31.743*{(20.9-15)/(20.9-9.10%)}=15.887 PPM@ 15% O2 HP HR From 40 CFR Part 60 Subpart JJJJ (31.743*(1.164*10^-3)*3483.735*(Run Time/60))/1328.382 = 0.097 G/HP-HR LB/HR from Grams LB/HR=0.097*1/453.6*1328.382=0.284 TPY TPY=0.3*4.38 = 1.243 TPY Horsepower 1328 = 1281.42857142857 - ((89.1 - 92) / ((89.1 - 71.9) / 25%))) * 1281.42857142857

8.0 Oxygen Calibration

- **8.1** Calibration error test; how do I confirm my analyzer calibration is correct? After the tester has assembled, prepared and calibrated the sampling system and analyzer, they conduct a 3-point analyzer calibration error test before the first run and again after any failed system bias test or failed drift test. They then introduce the low-, mid-, and high-level calibration gases sequentially in direct calibration mode. At each calibration gas level (low, mid, and high) the calibration error must be within ± 2.0 percent of the calibration span.
- **8.2** Initial system bias and system calibration error checks. Before sampling begins, it is determined whether the high-level or mid-level calibration gas best approximates the emissions and it is used as the upscale gas. The upscale gas is introduced at the probe upstream of all sample-conditioning components in system calibration mode.
 - (1) Next, zero gas is introduced as described above. The response must be within 0.5 percent of the upscale gas concentration.
 - (2) Low-level gas reading is observed until it has reached a final, stable value and the results are recorded. The measurement system will be operated at the normal sampling rate during all system bias checks.
 - (3) If the initial system bias specification is not met, corrective action is taken. The applicable calibration error test from Section 8.2.3 is repeated along with the initial system bias check until acceptable results are achieved, after which sampling will begin. The pre- and post-run system bias must be within ±5.0 percent of the calibration span for the low-level and upscale calibration gases.

8.3 Post-run system bias check and drift assessment - confirming that each sample collected is valid.

Sampling may be performed for multiple runs before performing the post-run bias or system calibration error check provided this test is passed at the conclusion of the group of runs. A failed final test in this case will invalidate all runs subsequent to the last passed test.

- (1) If the post-run system bias check is not passed, then the run is invalid. The problem is then diagnosed and fixed, then another calibration error test and system bias is passed before repeating the run.
- (2) After each run, the low-level and upscale drift is calculated, using Equation 7E–4 in Section 12.5 from EPA Method 7E. If the post-run low- and upscale bias checks are passed, but the low-or upscale drift exceeds the specification in Section 13.3, the run data are valid, but a 3-point calibration error test and a system bias check must be performed and passed prior to additional testing.

Table 8.1 Oxygen Calibration

Method 7E 3.4 To the extent practicable, the measured emissions should be between 20 to 100 percent of the selected calibration span. This may not be practicable in some cases of low concentration measurements or testing for compliance with an emission limit when emissions are substantially less than the limit.

		EPA Me	thod 3A QA Wo	orksheet						
	Concentration evel (%)		Certified Gas Concentration Mid-Level (%) Certified Gas Concentration High-Level (%)							
0.0	00%	9.0	00%	06%						
	(DIRECT) A	nalyzer Calibration Linerarity Check	Error (≤ 2%)		sampling for	nat you may risk multiple runs ing the post-run				
	Certified Concentration Value (%)	Direct Calibration Response (%)	Absolute Difference (%)	Analyzer Calibration Error (%)	bias provided you	ou pass this test on of the group runs				
Zero Gas %	0.00%	0.00%	0.00%	0.00%						
Mid-Level Gas %	9.00%	8.89%	-0.11%	0.52%						
High-Level Gas %	21.06%	20.85%	-0.21%	1.00%						
(SY	STEM) Calibration	Bias Checks (≤ 5%)	and Drift Checks (≤	3%)	Upscale Gas	9.00%				
Zero Offset	0.00%	Bia	Bias Pre Bias Post							
Span	21.06%	Initial	Values	Initial	Values					
	Analyzer Calibration Response (%)	System Calibration Response Pre (%)	System Bias (% of Span) Pre	System Calibration Response Post (%)	System Bias (% of Span) Post	Drift (% of Span)				
Zero Gas	0.00%	0%	0.00%	0%	0.00%	0.00%				
Upscale Gas	8.89%	8.74%	-0.71%	8.76%	-0.62%	0.09%				
	(SY	STEM) Calibration	Bias Checks (≤ 5%) a	and Drift Checks (≤	3%)					
	ntration (Run 1)	8.86%		(Cgas) Run 1		11%				
	ntration (Run 2)	8.82%	Effluent Gas	(Cgas) Run 2		9.07%				
Avg. Gas Conce	ntration (Run 3)	8.87%	Effluent Gas	12%						

Calibration Bottles				
Zero Gas	100% Nitrogen			
Mid-Level O2	9.00%			
High-Level O2	21.06%			

O2 QA/QC				
	Analyzer Direct Calibration Response	Certified bottle value %		
Zero Gas %	0.00%	0.00%		
Mid-Level Gas %	8.89%	9.00%		
High-Level Gas %	20.85%	21.06%		
	System Calibration Response Pre (%)			
Zero Gas	0%	Upscale Used		
Upscale Cal	8.74%	9.00%		
	System Calibration Response Post (%)			
Zero Gas	0%	Upscale Used		
Upscale Cal	8.76%	9.00%		

9.0 Engine Parameter Data Sheet



Company	Pioneer Natural Resources
Facility	Scharbauer Ranch 323-14H Tank Battery
Date	5/19/2021
Site Elevation (ft)	2,884
Unit ID	ENG 2 (K16-0436)
Make	Caterpillar
Model	3516B LE
Serial Number	JEF03385
Technician	Cory Garrison

	Run 1	Run 2	Run 3	Completed
Run Start Times	6:28	7:35	8:41	9:48
Engine Hours	17345	17346	17347	17348

		Engine Parameter Data				
	Run 1	Run 2	Run 3	Average		
Engine Speed (RPM)	1300	1299	1300	1300		
Intake Manifold Pressure (psi)	45.0	45.0	45.0	45.0		
Intake Manifold Temp °F	137.0	137.0	138.0	137.3		
Engine Load (BHP)	1328.38	1327.36	1328.38	1328.04		
Ambient Temp °F	64	63	62	63		
Humidity %	82	92	93	89		
Dew Point °F	58	60	60	59		
AFR Manufacturer/Type	Caterpillar	Caterpillar	Caterpillar	Caterpillar		
Suction Pressure (psi)	39.0	39.0	39.0	39.0		
Discharge Pressure (psi)	1225.0	1223.0	1222.0	1223.3		
Catalyst (Yes or No)	Yes	Yes	Yes	Yes		

<--- Not available on this unit</p>

10.0 QA/QC Results

Pre-test Baseline Results			
003 Carbon monoxide CO	Average:	0.6	
004 Nitrogen monoxide NO	Average:	0.0	Q
005 Nitrogen dioxide NO2	Average:	1.0	Α
201 NOx	Average:	1.0	/
202 VOC	Average:	1.2	<i>/</i>
223 Oxygen	Average:	0.0	Q
			С
CTS Direct to Analyzer			
CTS Bottle Concentration:	Average:	99.0	
CTS Compound Concentration Avg:	Average:	97.7	R
Tolerance:	Average:	4.9	е
Difference between measured and expected:	Average:	1.3	
			S
Pre-test System Zero			u
003 Carbon monoxide CO	Average:	1.9	
004 Nitrogen monoxide NO	Average:	0.0	
005 Nitrogen dioxide NO2	Average:	0.9	t
201 NOx	Average:	0.9	S
202 VOC	Average:	4.5	3
223 Oxygen	Average:	0.0	

Pre-test System CTS & Mechanical Response Time			
Mechanical Response Time:	73 seco	nds	
CTS Bottle Concentration:	Average:	99.0	
CTS Compound Concentration Avg:	Average:	97.9	
Tolerance:	Average:	4.9	
Difference between measured and expected:	Average:	1.1	

System (Equilibration) Response Time Target (Spike)			
Equilibration Response Time:	69 seco	onds	
Spike Reported:	Average:	252.7	
Spike Expected:	Average:	252.8	

System (Zero) Response Time	
System Zero Response Time:	65 seconds
System Response Time:	100 seconds

11.0 D6348 Annexes 1-8

D6348 Annex 1. Test Plan Requirements

Annex 1.2

The test quality objectives completed for the emissions test are demonstrated throughout Annexes 1, 2, 3, 4, 5, 6, 7 & 8 as layed out per ASTM D6348-03. All reference methods, pre-test and post test procedures were within acceptable limits. Data generated during the pre-test and post-test procedures are summarized below in order of the distinctive Annex.

Three 01:00 hour - test runs were performed. The final analyte concentrations are the average of each test run. Data was taken at 20 second intervals. Each 20 second measurement was the average of 200 scans.

Annex Table 1.2.1 Certified Calibration Bottle Concentrations

Bottle	Expiration	NO2	Ethylene		O2 (%)
CC511378	10/9/23	101.30			9.00%
CC420697	11/6/23		98.96		
CC317205	12/16/27				21.06%

Cylinder # CC48394 Expiration: 10-12-28					
	Propane	со	NO	SF6	
Bottle Value	252.80	495.60	254.20	10.15	
Analyzer System Response	252.70	499.50	253.60	10.13	
Percent Difference	0.04%	0.79%	0.24%	0.20%	

Annex Table 1.2.2 Measurement System Capabilities

Parameter Measured	Gas	Concentration (ppm)	Path Length	Equilibration Time	Dilution Factor	% Recovery
Path Length	Ethylene	97.670	4.935			
	Propane	248.100				
	SF6	9.960				
Spike Direct	СО	491.100				
	NO	251.800				
	NO2	100.500				
Mechanical Response Time	Ethylene	97.850		73 seconds		
	Propane	252.700				
	SF6	10.130		69 seconds		
Analyzer Response	СО	499.500				
Кезропзе	NO	253.600				
	NO2	99.800				
A					6.73%	96.12%
Analyte Spike Recovery	Propane & SF6				6.53%	106.35%
necovery					6.53%	101.74%
System Zero	Nitrogen			65 seconds		
	Propane	246.800				
Post Spike System	СО	485.600				
1 03t Spike System	NO	247.900				
	NO2	103.590				

Annex 1.3

Annex Table 1.3.1 Test Specific Target Analytes and Data Quality Objectives

Compounds	Infrared Analysis Region (cm-1)	Expected Concentration Range	Measurement System Achievable Minimum Detectable Concentrations	Required Measurement System Accuracy and Precision for Test Application	
СО	2000-2200	0-1200 ppm	0.16267 ppm	4 ppm	
NO	1875-2138	0-1000 ppm	0.4007 ppm	2 ppm	
NO2	2700-2950	0-100 ppm	0.4899 ppm	2 ppm	
	2600-3200		1 05 30 nnm Total		
VOC	910-1150	0-100 ppm	1.8520 ppm Total VOC's	1 ppm per VOC	
	2550-2950		VOC 3		
CH2O	2550-2850	0-100 ppm	0.7878 ppm	1 ppm	
Interfering Compounds	* CO is analyzed in	d in a separate analysis region than CO2 and H2O			
CO ₂	926-1150	0-10%		n/a	
Water Vapor	3200-3401	0-22%	0.20%	n/a	

^{*} VOCs compiled of Acetaldehyde, Ethylene, Hexane, and Propane

Annex 1.4

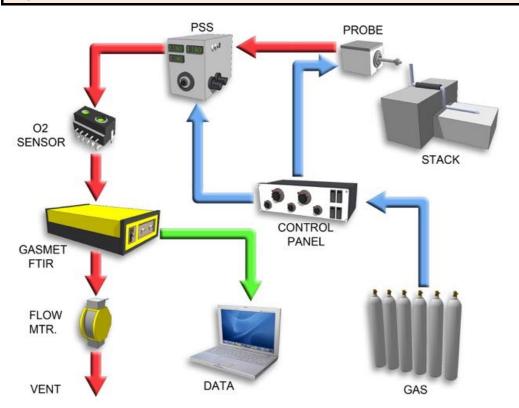
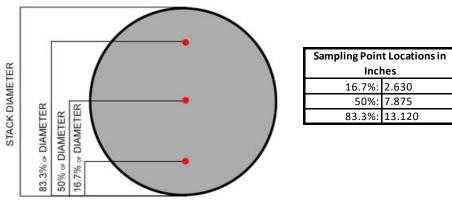


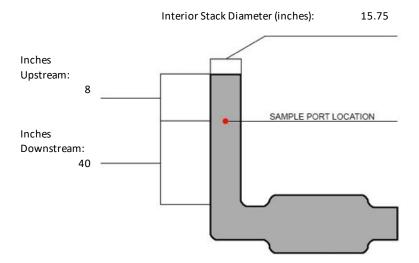
Figure Annex 1.4.1 Sampling Train

The testing instrumentation is housed in an enclosed vehicle which is located approximately 45 feet from the source. A heated sample line (sixty feet in length) is attached to the inlet of analyzer system and the source effluent discharges through the analyzer outlet.



TRI-PROBE SAMPLE POINT LOCATIONS AS PERCENTAGE OF STACK DIAMETER

Figure Annex 1.4.2 Sampling Points



SAMPLE PORT LOCATION DETERMINED BY DISTANCE FROM DISTURBANCE

Figure Annex 1.4.3 Sample Port Location

Pressure @ Sampling Point (Pg "H2O):	0.49
Temperature @ Sampling Point (Deg F):	625.58
Stack Gas Dry Volumetric Flow Rate (scf/hr):	133245.93
H2O%d @ Sampling Point:	12.18
CO2%d @ Sampling Point:	5.75

D6348 Annex 2. Determination of FTIR Measurement System Minimum Detectable Concentrations (MDC#1

Target Analyte	Results (ppm)
CO	0.2603
NO	0.6410
NO2	1.3387
Total VOC's	2.3011
Ethylene	0.3011
Propane	0.5906
Hexane	0.3030
Acetaldehyde	1.1064
Formaldehyde	1.0691

$$NEA_{rms}^{\ m} = \sqrt{\frac{1}{n} \sum_{j=1}^{N_m} \left(NEA_i^m\right)^2}$$

$$REF_{rms}^{\ m} = \sqrt{\frac{1}{n} \sum_{j=1}^{N_m} \left(REF_i^m\right)^2}$$

$$MDC\#1 = \frac{NEA_{rms}^{\ m}}{REF_{rms}} * \frac{C_{ref}L_{ref}}{L_{cell}}$$

D6348 Annex 3. FTIR Reference Spectra

Calibration Transfer Standard	Expected	Measured	Path Length	Validated
Ethylene	98.96	97.67	4.935	Passed

Within 5% of certified bottle value demonstrating Linearity and Pathlength

D6348 Annex 4. Required Pre-Test Procedures

Annex Table 4.1 Measurement System Capabilities

Parameter Measured	Gas	Concentration (ppm)	Path Length	Equilibration Time	Dilution Factor	% Recovery
Path Length	Ethylene	97.670	4.935			
	Propane	248.100				
	SF6	9.960				
Spike Direct	СО	491.100				
	NO	251.800				
	NO2	100.500				
Mechanical Response Time	Ethylene	97.850		73 seconds		
	Propane	252.700		69 seconds		
Custom Dosnonso	SF6	10.130				
System Response Time	CO	499.500		09 seconds		
Time	NO	253.600				
	NO2	99.800				
A l					6.73%	96.12%
Analyte Spike Recovery	Propane & SF6				6.53%	106.35%
Recovery					6.53%	101.74%
System Zero	Nitrogen			65 seconds		
	Propane	246.800				
Burt Suite Suite	СО	485.600				
Post Spike System	NO	247.900				
	NO2	103.590				

D6348 Annex 5. Analyte Spiking Technique

Parameter	Gas	Concentration	Measured	% Difference	Specification	Validated
	Propane	252.800	248.100	1.86%	+/- 2%	Pass
	SF6	10.150	9.960	1.87%	+/- 2%	Pass
Cailea Direat	CO	495.600	491.100	0.91%	+/- 2%	Pass
Spike Direct	NO	254.200	251.800	0.94%	+/- 2%	Pass
	NO2	101.300	100.500	0.79%	+/- 2%	Pass
			_			

Spike Run 1 via the System						
9	Source Output Spike Average Dilution Factor Expected % Recovery					Specification
Propane	1.220	17.440		18.144	96.12%	70-130%
SF6	0.050	0.670	6.73%			<10%

Spike Run 2 via the System						
	Source Output Spike Average Dilution Factor Expected % Recovery				Specification	
Propane	0.960	18.500		17.395	106.35%	70-130%
SF6		0.650	6.53%			<10%

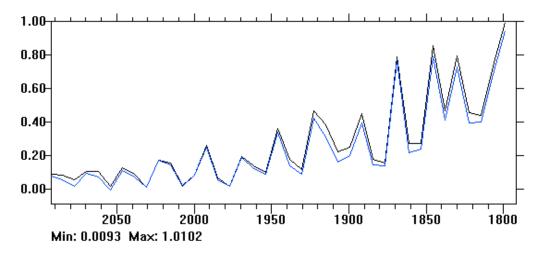
Spike Run 3 via the System						
9	Source Output	Spike Average	Dilution Factor	Expected	% Recovery	Specification
Propane	1.530	18.240		17.928	101.74%	70-130%
SF6		0.650	6.53%			<10%

D6348 Annex 6. Determination of System Performance Parameters

Noise Equivalent Absorbance (NEA)

RMS High 0.000312 RMS Mid 0.000096 RMS Low 0.000119

Line Position: Demonstrating the peak positions align correctly (Manual Comparison +/-20%)

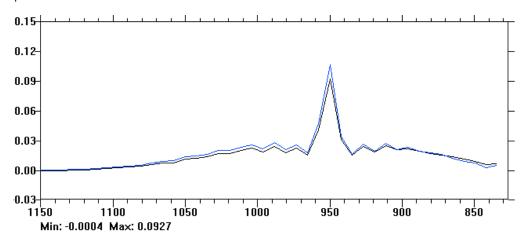


Resolution

The Gasmet GICCOR (Genzel Interferometer with Cube Corner Retroreflectors) interferometer is specially designed for maximum optical throughput and maximum signal to noise ratio of 7.72 (cm-1) remaining stable with any vibration and temperature changes.

Detector Linerarity

The Gasmet DX4000 is a low resolution spectrometer where the aperture is fixed to a maximum angle setting and the detector linearity was tested with an alternate approach. A three point linearity of the CTS gas was performed and validated.



D6348 Annex 7. Preparation of Analytical Quantification Algorithm

 $The \ analytical \ accuracy of the \ quantification \ algorithm \ is \ satisfied \ via \ the \ results \ from \ Annex \ 5, per \ Annex \ 7.6$

D6348 Annex 8. Post Test Quality Assurance/Quality Control Procedures

POST CTS System Check:	
CTS Bottle Concentration:	98.96
CTS Sample Concentration Average:	96.50
Difference between measured and expected:	2.46
Tolerance:	4.95

12.0 RMGuide Report for:

Pioneer Natural Resources Scharbauer Ranch 323-14H Tank Battery JJJJ

CTS Bottle Concentration:	98.96
Spike Bottle Concentration:	252.80
SF6 Bottle Concentration:	10.15
System Response Time:	100 seconds
Minimum Response Time:	100 seconds

	Step: 06 PRE-TEST Baseline Results:						
Water Vapor H2O	Average:	-0.18	Residual:	0.0007			
Carbon monoxide CO	Average:	0.57	Residual:	0.0006			
Nitrogen monoxide NO	Average:	0.00	Residual:	0.0012			
Nitrogen dioxide NO2	Average:	1.02	Residual:	0.0002			
Propane C3H8	Average:	0.07	Residual:	0.0003			
Sulfur hexafluoride SF6	Average:	0.00	Residual:	0.0015			
Ethylene C2H4	Average:	0.41	Residual:	0.0011			
Methane CH4	Average:	1.42	Residual:	0.0005			
Nitrous oxide N2O	Average:	0.02	Residual:	0.0006			
Carbon dioxide CO2	Average:	0.02	Residual:	0.0010			
Ammonia NH3	Average:	0.00	Residual:	0.0011			
Ethane C2H6	Average:	0.00	Residual:	0.0009			
Hexane C6H14	Average:	0.01	Residual:	0.0003			
Acetaldehyde C2H4O	Average:	0.68	Residual:	0.0003			
NOx	Average:	1.02	Residual:	0.0012			
voc	Average:	1.17	Residual:	0.0011			
Ambient pressure	Average:	912.00	Residual:	0.0000			
Oxygen	Average:	0.00	Residual:	0.0000			
Cell temperature	Average:	180.00	Residual:	0.0000			
Interferometer temperature	Average:	34.60	Residual:	0.0000			
Detector temperature	Average:	37.12	Residual:	0.0000			
IFG Center	Average:	2409.00	Residual:	0.0000			
Source intensity	Average:	92.00	Residual:	0.0000			
Electronics temperature	Average:		Residual:				
External temperature	Average:	25.26	Residual:	0.0000			

Step:07 CTS Direct to Analyzer:				
CTS Bottle Concentration:	98.96			
CTS Concentration Average:	97.67			
Tolerance:	4.948			
Difference between measured and expected	1.29			

Step: 08 PRE-TEST System Zero:				
Water vapor H2O	Average:	-0.01	Residual:	0.0022
Carbon monoxide CO	Average:	1.91	Residual:	0.0006
Nitrogen monoxide NO	Average:	0.00	Residual:	0.0012
Nitrogen dioxide NO2	Average:	0.87	Residual:	0.0002
Propane C3H8	Average:	0.00	Residual:	0.0014
Sulfur hexafluoride SF6	Average:	0.00	Residual:	0.0060
Ethylene C2H4	Average:	1.42	Residual:	0.0035
Methane CH4	Average:	2.75	Residual:	0.0003
Nitrous oxide N2O	Average:	0.09	Residual:	0.0006
Carbon dioxide CO2	Average:	0.23	Residual:	0.0034
Ammonia NH3	Average:	0.00	Residual:	0.0035
Ethane C2H6	Average:	0.00	Residual:	0.0020
Hexane C6H14	Average:	0.12	Residual:	0.0005
Acetaldehyde C2H4O	Average:	3.00	Residual:	0.0007
NOx	Average:	0.87	Residual:	0.0012
voc	Average:	4.54	Residual:	0.0035
Ambient pressure	Average:	910.67	Residual:	0.0000
Oxygen	Average:	0.00	Residual:	0.0000
Cell temperature	Average:	180.00	Residual:	0.0000
Interferometer temperature	Average:	37.34	Residual:	0.0000
Detector temperature	Average:	37.14	Residual:	0.0000
IFG Center	Average:	2415.33	Residual:	0.0000
Source intensity	Average:	92.67	Residual:	0.0000
External temperature	Average:	25.31	Residual:	0.0000

Step: 09 PRE-TEST System CTS & Mechanical Response Time			
Mechanical Response Time: 73 se			
CTS Bottle Concentration:	98.96		
CTS Concentration Average:	97.85		
Tolerance:	4.948		
Difference bettween measured and expected	1.11		

Step: 10 System(Equilibration) Response Time Target (Spike)				
Equilibration Response Time: 69 seconds				
Spike Reported:	252.7			
Spike Expected:	252.80			

Step: 11 System(Zero) Response Time				
System Zero Response Time:	65 seconds			
System Response Time:	100 seconds			
W-t	A	0.00	Residual:	0.0022
Water vapor H2O Carbon monoxide CO	Average:	0.00	Residual:	0.0022
	Average:			
Nitrogen monoxide NO	Average:	0.00	Residual:	0.0011
Nitrogen dioxide NO2	Average:	0.00	Residual:	0.0002
Propane C3H8	Average:	0.00	Residual:	0.0008
Sulfur hexafluoride SF6	Average:	0.01	Residual:	0.0064
Ethylene C2H4	Average:	0.00	Residual:	0.0038
Methane CH4	Average:	3.52	Residual:	0.0006
Nitrous oxide N2O	Average:	0.10	Residual:	0.0006
Carbon dioxide CO2	Average:	0.27	Residual:	0.0035
Ammonia NH3	Average:	0.00	Residual:	0.0038
Ethane C2H6	Average:	0.00	Residual:	0.0020
Hexane C6H14	Average:	0.00	Residual:	0.0006
Acetaldehyde C2H4O	Average:	0.00	Residual:	0.0007
NOx	Average:	0.00	Residual:	0.0011
VOC	Average:	0.00	Residual:	0.0038
Ambient pressure	Average:	911.00	Residual:	0.0000
Oxygen	Average:	0.00	Residual:	0.0000
Cell temperature	Average:	180.00	Residual:	0.0000
Interferometer temperature	Average:	38.39	Residual:	0.0000
Detector temperature	Average:	37.14	Residual:	0.0000
IFG Center	Average:	2390.33	Residual:	0.0000
Source intensity	Average:	93.00	Residual:	0.0000
External temperature	Average:	25.68	Residual:	0.0000

Step: 12 SOURCE GAS 1A					
Water vapor H2O	Average:	11.62	Residual:	0.0091	
Carbon monoxide CO	Average:	29.61	Residual:	0.0070	
Nitrogen monoxide NO	Average:	77.06	Residual:	0.0138	
Nitrogen dioxide NO2	Average:	11.96	Residual:	0.0023	
Propane C3H8	Average:	1.22	Residual:	0.0031	
Sulfur hexafluoride SF6	Average:	0.05	Residual:	0.0036	
Ethylene C2H4	Average:	11.30	Residual:	0.0031	
Methane CH4	Average:	1061.25	Residual:	0.0185	
Nitrous oxide N2O	Average:	0.00	Residual:	0.0071	
Carbon dioxide CO2	Average:	5.79	Residual:	0.0026	
Ammonia NH3	Average:	0.00	Residual:	0.0031	
Ethane C2H6	Average:	57.53	Residual:	0.0026	
Hexane C6H14	Average:	1.00	Residual:	0.0026	
Acetaldehyde C2H4O	Average:	5.36	Residual:	0.0030	
NOx	Average:	89.02	Residual:	0.0138	
VOC	Average:	18.88	Residual:	0.0032	
Ambient pressure	Average:	910.89	Residual:	0.0000	
Oxygen	Average:	7.88	Residual:	0.0000	
Cell temperature	Average:	180.01	Residual:	0.0000	
Interferometer temperature	Average:	40.78	Residual:	0.0000	
Detector temperature	Average:	37.08	Residual:	0.0000	
IFG Center	Average:	2386.59	Residual:	0.0000	
Source intensity	Average:	93.00	Residual:	0.0000	
External temperature	Average:	28.95	Residual:	0.0000	

Step: 13 SPIKE GAS- A				
Water vapor H2O	Average:	10.97	Residual:	0.0092
Carbon monoxide CO	Average:	60.13	Residual:	0.0067
Nitrogen monoxide NO	Average:	89.31	Residual:	0.0134
Nitrogen dioxide NO2	Average:	6.52	Residual:	0.0024
Propane C3H8	Average:	17.44	Residual:	0.0025
Sulfur hexafluoride SF6	Average:	0.67	Residual:	0.0033
Ethylene C2H4	Average:	12.39	Residual:	0.0027
Methane CH4	Average:	998.06	Residual:	0.0178
Nitrous oxide N2O	Average:	0.00	Residual:	0.0068
Carbon dioxide CO2	Average:	5.76	Residual:	0.0026
Ammonia NH3	Average:	0.00	Residual:	0.0027
Ethane C2H6	Average:	48.66	Residual:	0.0025
Hexane C6H14	Average:	1.77	Residual:	0.0025
Acetaldehyde C2H4O	Average:	5.40	Residual:	0.0026
NOx	Average:	95.84	Residual:	0.0134
VOC	Average:	37.00	Residual:	0.0027
Ambient pressure	Average:	910.00	Residual:	0.0000
Oxygen	Average:	7.38	Residual:	0.0000
Cell temperature	Average:	180.00	Residual:	0.0000
Interferometer temperature	Average:	41.33	Residual:	0.0000
Detector temperature	Average:	37.07	Residual:	0.0000
IFG Center	Average:	2371.67	Residual:	0.0000
Source intensity	Average:	93.00	Residual:	0.0000
External temperature	Average:	29.49	Residual:	0.0000

Step: 14 SOURCE GAS 02-A					
Water vapor H2O	Average:	12.06	Residual:	0.0097	
Carbon monoxide CO	Average:	26.36	Residual:	0.0067	
Nitrogen monoxide NO	Average:	74.87	Residual:	0.0135	
Nitrogen dioxide NO2	Average:	15.39	Residual:	0.0025	
Propane C3H8	Average:	0.43	Residual:	0.0028	
Sulfur hexafluoride SF6	Average:	0.01	Residual:	0.0029	
Ethylene C2H4	Average:	11.70	Residual:	0.0027	
Methane CH4	Average:	1051.30	Residual:	0.0187	
Nitrous oxide N2O	Average:	0.00	Residual:	0.0068	
Carbon dioxide CO2	Average:	5.72	Residual:	0.0019	
Ammonia NH3	Average:	0.00	Residual:	0.0027	
Ethane C2H6	Average:	57.81	Residual:	0.0028	
Hexane C6H14	Average:	0.78	Residual:	0.0028	
Acetaldehyde C2H4O	Average:	5.21	Residual:	0.0028	
NOx	Average:	90.26	Residual:	0.0135	
VOC	Average:	18.12	Residual:	0.0030	
Ambient pressure	Average:	910.54	Residual:	0.0000	
Oxygen	Average:	7.74	Residual:	0.0000	
Cell temperature	Average:	180.03	Residual:	0.0000	
Interferometer temperature	Average:	42.34	Residual:	0.0000	
Detector temperature	Average:	37.05	Residual:	0.0000	
IFG Center	Average:	2367.06	Residual:	0.0000	
Source intensity	Average:	93.00	Residual:	0.0000	
External temperature	Average:	30.46	Residual:	0.0000	

Step: 15 BASELINE GAS 01-B				
Water vapor H2O	Average:	0.00	Residual:	0.0013
Carbon monoxide CO	Average:	1.22	Residual:	0.0004
Nitrogen monoxide NO	Average:	0.00	Residual:	0.0011
Nitrogen dioxide NO2	Average:	0.11	Residual:	0.0002
Propane C3H8	Average:	0.00	Residual:	0.0006
Sulfur hexafluoride SF6	Average:	0.00	Residual:	0.0039
Ethylene C2H4	Average:	0.57	Residual:	0.0029
Methane CH4	Average:	2.46	Residual:	0.0003
Nitrous oxide N2O	Average:	0.06	Residual:	0.0004
Carbon dioxide CO2	Average:	0.38	Residual:	0.0027
Ammonia NH3	Average:	0.00	Residual:	0.0028
Ethane C2H6	Average:	0.00	Residual:	0.0004
Hexane C6H14	Average:	0.12	Residual:	0.0003
Acetaldehyde C2H4O	Average:	1.06	Residual:	0.0004
NOx	Average:	0.11	Residual:	0.0011
VOC	Average:	1.75	Residual:	0.0029
Ambient pressure	Average:	911.00	Residual:	0.0000
Oxygen	Average:	0.00	Residual:	0.0000
Cell temperature	Average:	180.00	Residual:	0.0000
Interferometer temperature	Average:	43.15	Residual:	0.0000
Detector temperature	Average:	37.04	Residual:	0.0000
IFG Center	Average:	2395.67	Residual:	0.0000
Source intensity	Average:	93.00	Residual:	0.0000
External temperature	Average:	31.22	Residual:	0.0000

Step: 16 SOURCE GAS 01-B					
Water vapor H2O	Average:	12.27	Residual:	0.0099	
Carbon monoxide CO	Average:	26.09	Residual:	0.0064	
Nitrogen monoxide NO	Average:	75.59	Residual:	0.0133	
Nitrogen dioxide NO2	Average:	17.94	Residual:	0.0025	
Propane C3H8	Average:	0.96	Residual:	0.0028	
Sulfur hexafluoride SF6	Average:	0.00	Residual:	0.0029	
Ethylene C2H4	Average:	11.83	Residual:	0.0027	
Methane CH4	Average:	1070.03	Residual:	0.0192	
Nitrous oxide N2O	Average:	0.00	Residual:	0.0064	
Carbon dioxide CO2	Average:	5.80	Residual:	0.0020	
Ammonia NH3	Average:	0.00	Residual:	0.0028	
Ethane C2H6	Average:	58.60	Residual:	0.0028	
Hexane C6H14	Average:	0.65	Residual:	0.0028	
Acetaldehyde C2H4O	Average:	5.52	Residual:	0.0027	
NOx	Average:	93.53	Residual:	0.0133	
VOC	Average:	18.96	Residual:	0.0028	
Ambient pressure	Average:	911.00	Residual:	0.0000	
Oxygen	Average:	7.82	Residual:	0.0000	
Cell temperature	Average:	180.05	Residual:	0.0000	
Interferometer temperature	Average:	43.66	Residual:	0.0000	
Detector temperature	Average:	37.03	Residual:	0.0000	
IFG Center	Average:	2380.07	Residual:	0.0000	
Source intensity	Average:	93.01	Residual:	0.0000	
External temperature	Average:	31.70	Residual:	0.0000	

Step: 17 SPIKE GAS- B				
Water vapor H2O	Average:	11.56	Residual:	0.0093
Carbon monoxide CO	Average:	57.69	Residual:	0.0061
Nitrogen monoxide NO	Average:	87.49	Residual:	0.0128
Nitrogen dioxide NO2	Average:	9.80	Residual:	0.0024
Propane C3H8	Average:	18.50	Residual:	0.0023
Sulfur hexafluoride SF6	Average:	0.65	Residual:	0.0027
Ethylene C2H4	Average:	12.19	Residual:	0.0025
Methane CH4	Average:	1000.58	Residual:	0.0184
Nitrous oxide N2O	Average:	0.00	Residual:	0.0061
Carbon dioxide CO2	Average:	5.76	Residual:	0.0023
Ammonia NH3	Average:	0.00	Residual:	0.0025
Ethane C2H6	Average:	50.33	Residual:	0.0023
Hexane C6H14	Average:	1.22	Residual:	0.0023
Acetaldehyde C2H4O	Average:	5.53	Residual:	0.0027
NOx	Average:	97.30	Residual:	0.0128
VOC	Average:	37.44	Residual:	0.0027
Ambient pressure	Average:	911.00	Residual:	0.0000
Oxygen	Average:	7.25	Residual:	0.0000
Cell temperature	Average:	180.00	Residual:	0.0000
Interferometer temperature	Average:	44.10	Residual:	0.0000
Detector temperature	Average:	37.02	Residual:	0.0000
IFG Center	Average:	2368.33	Residual:	0.0000
Source intensity	Average:	93.00	Residual:	0.0000
External temperature	Average:	32.12	Residual:	0.0000

Step: 18 SOURCE GAS 02-B					
Water vapor H2O	Average:	12.70	Residual:	0.0102	
Carbon monoxide CO	Average:	25.54	Residual:	0.0062	
Nitrogen monoxide NO	Average:	73.53	Residual:	0.0131	
Nitrogen dioxide NO2	Average:	15.74	Residual:	0.0026	
Propane C3H8	Average:	1.50	Residual:	0.0028	
Sulfur hexafluoride SF6	Average:	0.01	Residual:	0.0028	
Ethylene C2H4	Average:	11.77	Residual:	0.0026	
Methane CH4	Average:	1052.69	Residual:	0.0197	
Nitrous oxide N2O	Average:	0.00	Residual:	0.0062	
Carbon dioxide CO2	Average:	5.71	Residual:	0.0019	
Ammonia NH3	Average:	0.00	Residual:	0.0026	
Ethane C2H6	Average:	57.96	Residual:	0.0028	
Hexane C6H14	Average:	0.56	Residual:	0.0028	
Acetaldehyde C2H4O	Average:	5.50	Residual:	0.0027	
NOx	Average:	89.27	Residual:	0.0131	
VOC	Average:	19.33	Residual:	0.0028	
Ambient pressure	Average:	911.29	Residual:	0.0000	
Oxygen	Average:	7.62	Residual:	0.0000	
Cell temperature	Average:	180.01	Residual:	0.0000	
Interferometer temperature	Average:	44.61	Residual:	0.0000	
Detector temperature	Average:	37.01	Residual:	0.0000	
IFG Center	Average:	2359.41	Residual:	0.0000	
Source intensity	Average:	93.61	Residual:	0.0000	
External temperature	Average:	32.69	Residual:	0.0000	

Step: 19 BASELINE GAS 01-C				
Water vapor H2O	Average:	0.00	Residual:	0.0011
Carbon monoxide CO	Average:	1.17	Residual:	0.0004
Nitrogen monoxide NO	Average:	0.00	Residual:	0.0011
Nitrogen dioxide NO2	Average:	0.03	Residual:	0.0004
Propane C3H8	Average:	0.00	Residual:	0.0005
Sulfur hexafluoride SF6	Average:	0.00	Residual:	0.0036
Ethylene C2H4	Average:	0.40	Residual:	0.0028
Methane CH4	Average:	2.65	Residual:	0.0004
Nitrous oxide N2O	Average:	0.06	Residual:	0.0004
Carbon dioxide CO2	Average:	0.40	Residual:	0.0025
Ammonia NH3	Average:	0.00	Residual:	0.0027
Ethane C2H6	Average:	0.12	Residual:	0.0003
Hexane C6H14	Average:	0.18	Residual:	0.0003
Acetaldehyde C2H4O	Average:	1.04	Residual:	0.0004
NOx	Average:	0.03	Residual:	0.0011
VOC	Average:	1.62	Residual:	0.0028
Ambient pressure	Average:	912.00	Residual:	0.0000
Oxygen	Average:	0.00	Residual:	0.0000
Cell temperature	Average:	180.00	Residual:	0.0000
Interferometer temperature	Average:	45.14	Residual:	0.0000
Detector temperature	Average:	37.00	Residual:	0.0000
IFG Center	Average:	2347.67	Residual:	0.0000
Source intensity	Average:	94.00	Residual:	0.0000
External temperature	Average:	33.21	Residual:	0.0000

Step: 20 SOURCE GAS 01-C				
Water vapor H2O	Average:	12.32	Residual:	0.0096
Carbon monoxide CO	Average:	26.14	Residual:	0.0058
Nitrogen monoxide NO	Average:	75.64	Residual:	0.0125
Nitrogen dioxide NO2	Average:	12.42	Residual:	0.0024
Propane C3H8	Average:	1.53	Residual:	0.0024
Sulfur hexafluoride SF6	Average:	0.00	Residual:	0.0028
Ethylene C2H4	Average:	11.85	Residual:	0.0027
Methane CH4	Average:	1068.36	Residual:	0.0194
Nitrous oxide N2O	Average:	0.00	Residual:	0.0058
Carbon dioxide CO2	Average:	5.77	Residual:	0.0019
Ammonia NH3	Average:	0.00	Residual:	0.0027
Ethane C2H6	Average:	58.76	Residual:	0.0024
Hexane C6H14	Average:	0.66	Residual:	0.0024
Acetaldehyde C2H4O	Average:	5.40	Residual:	0.0026
NOx	Average:	88.06	Residual:	0.0125
VOC	Average:	19.44	Residual:	0.0027
Ambient pressure	Average:	912.67	Residual:	0.0000
Oxygen	Average:	7.83	Residual:	0.0000
Cell temperature	Average:	179.99	Residual:	0.0000
Interferometer temperature	Average:	45.01	Residual:	0.0000
Detector temperature	Average:	37.00	Residual:	0.0000
IFG Center	Average:	2346.61	Residual:	0.0000
Source intensity	Average:	94.00	Residual:	0.0000
External temperature	Average:	33.02	Residual:	0.0000

Step: 21 SPIKE GAS- C				
Water vapor H2O	Average:	11.34	Residual:	0.0089
Carbon monoxide CO	Average:	58.36	Residual:	0.0057
Nitrogen monoxide NO	Average:	90.24	Residual:	0.0121
Nitrogen dioxide NO2	Average:	7.08	Residual:	0.0022
Propane C3H8	Average:	18.24	Residual:	0.0020
Sulfur hexafluoride SF6	Average:	0.65	Residual:	0.0027
Ethylene C2H4	Average:	11.85	Residual:	0.0023
Methane CH4	Average:	1003.56	Residual:	0.0181
Nitrous oxide N2O	Average:	0.00	Residual:	0.0057
Carbon dioxide CO2	Average:	5.73	Residual:	0.0018
Ammonia NH3	Average:	0.00	Residual:	0.0022
Ethane C2H6	Average:	50.67	Residual:	0.0020
Hexane C6H14	Average:	1.40	Residual:	0.0020
Acetaldehyde C2H4O	Average:	5.44	Residual:	0.0024
NOx	Average:	97.32	Residual:	0.0121
VOC	Average:	36.92	Residual:	0.0025
Ambient pressure	Average:	913.00	Residual:	0.0000
Oxygen	Average:	7.37	Residual:	0.0000
Cell temperature	Average:	180.00	Residual:	0.0000
Interferometer temperature	Average:	43.91	Residual:	0.0000
Detector temperature	Average:	37.02	Residual:	0.0000
IFG Center	Average:	2364.33	Residual:	0.0000
Source intensity	Average:	94.00	Residual:	0.0000
External temperature	Average:	31.76	Residual:	0.0000

Step: 22 SOURCE GAS 02-C				
Water vapor H2O	Average:	12.08	Residual:	0.0093
Carbon monoxide CO	Average:	26.65	Residual:	0.0059
Nitrogen monoxide NO	Average:	78.35	Residual:	0.0124
Nitrogen dioxide NO2	Average:	10.14	Residual:	0.0025
Propane C3H8	Average:	0.53	Residual:	0.0026
Sulfur hexafluoride SF6	Average:	0.01	Residual:	0.0027
Ethylene C2H4	Average:	11.03	Residual:	0.0023
Methane CH4	Average:	1062.74	Residual:	0.0186
Nitrous oxide N2O	Average:	0.00	Residual:	0.0060
Carbon dioxide CO2	Average:	5.69	Residual:	0.0019
Ammonia NH3	Average:	0.00	Residual:	0.0020
Ethane C2H6	Average:	58.55	Residual:	0.0025
Hexane C6H14	Average:	0.82	Residual:	0.0025
Acetaldehyde C2H4O	Average:	4.64	Residual:	0.0028
NOx	Average:	88.49	Residual:	0.0124
VOC	Average:	17.02	Residual:	0.0028
Ambient pressure	Average:	912.39	Residual:	0.0000
Oxygen	Average:	7.75	Residual:	0.0000
Cell temperature	Average:	180.03	Residual:	0.0000
Interferometer temperature	Average:	42.49	Residual:	0.0000
Detector temperature	Average:	37.05	Residual:	0.0000
IFG Center	Average:	2383.53	Residual:	0.0000
Source intensity	Average:	93.21	Residual:	0.0000
External temperature	Average:	30.39	Residual:	0.0000

Step: 23 BASELINE GAS 02-C				
Water vapor H2O	Average:	0.00	Residual:	0.0011
Carbon monoxide CO	Average:	1.11	Residual:	0.0004
Nitrogen monoxide NO	Average:	0.00	Residual:	0.0010
Nitrogen dioxide NO2	Average:	0.28	Residual:	0.0003
Propane C3H8	Average:	0.06	Residual:	0.0003
Sulfur hexafluoride SF6	Average:	0.00	Residual:	0.0036
Ethylene C2H4	Average:	0.38	Residual:	0.0026
Methane CH4	Average:	1.83	Residual:	0.0004
Nitrous oxide N2O	Average:	0.03	Residual:	0.0004
Carbon dioxide CO2	Average:	0.37	Residual:	0.0025
Ammonia NH3	Average:	0.00	Residual:	0.0026
Ethane C2H6	Average:	0.00	Residual:	0.0005
Hexane C6H14	Average:	0.14	Residual:	0.0003
Acetaldehyde C2H4O	Average:	0.85	Residual:	0.0003
NOx	Average:	0.28	Residual:	0.0010
VOC	Average:	1.43	Residual:	0.0026
Ambient pressure	Average:	912.00	Residual:	0.0000
Oxygen	Average:	0.00	Residual:	0.0000
Cell temperature	Average:	180.00	Residual:	0.0000
Interferometer temperature	Average:	41.46	Residual:	0.0000
Detector temperature	Average:	37.07	Residual:	0.0000
IFG Center	Average:	2398.33	Residual:	0.0000
Source intensity	Average:	93.00	Residual:	0.0000
External temperature	Average:	29.53	Residual:	0.0000

Step: 24 POST CTS Direct to Analyzer:				
CTS Bottle Concentration:	98.96			
CTS Concentration Average:	96.5			
Tolerance:	4.948			
Difference between measured and expected:	2.46			

13.0 Signature Page

R0

Job/File Name:

Pioneer Natural Resources; Scharbauer Ranch 323-14H Tank Battery;

ENG 2 (K16-0436); JJJJ;



We certify that based on review of test data, knowledge of those individuals directly responsible for conducting this test, we believe the submitted information to be accurate and complete.

Company:	G.A.S. Inc.	Date:	5/26/21
Print Name:	Mike Chapel		
Title:	Director of Stack Testing		
Signature:	Mike Chapel		
Phone Number:	580-225-0403		

Company:	G.A.S. Inc.	Date:	5/26/21
Print Name:	Cory Garrison		
Title:	Emissions Specialist		

Company:	Pioneer Natural Resources	
Print Name:	Efrain Vizcaino	Date: 5/26/21
Signature:	-0	
Title:	Engine Compliance Tech III	
Phone Number:	432-254-1347	

Appendices

Spike (5 Gas)



Airgas Specialty Gases Airgas USA, LLC 12722 S. Wentworth Ave. Chicago, IL 60628 Airgas.com

CERTIFICATE OF ANALYSIS Grade of Product: EPA Protocol

Reference Number: 54-401922301-1 Cylinder Volume: 147.0 CF Cylinder Pressure: 2015 PSIG Valve Outlet: 660 E05NI94E15AC014 Part Number: Cylinder Number: Laboratory: PGVP Number: CC48394 124 - Chicago (SAP) - IL B12020 CO,CO2,NO,NOX,PPN,BALN Gas Code: Certification Date: Oct 12, 2020

Certification Date: Oct 12, 2020

Expiration Date: Oct 12, 2028

Certification performed in accordance with "EPA Traceability Protocol for Assay and Certification of Gaseous Calibration Standards (May 2012)" document EPA 600/R-12/S31, using the assay procedures listed. Analytical Methodology does not require correction for analytical interference. This cylinder has a total analytical uncertainty as stated below with a confidence level of 95%. There are no significant impurities which affect the use of this calibration mixture. All concentrations are on a mole/mole basis unless otherwise noted.

Do Not Use This Cylinder below 100 psig. Le. O.7 megapascals.

Bo Not obs This Cylinder bolow Too poig, i.e. o. Thiographicale.						
ANALYTICAL RESULTS						
Component	Requested Concentration	Actual Concentration	Protocol Method	Total Relative Uncertainty	Assay Dates	
NOX	250.0 PPM	254.8 PPM	G1	+/- 0.9% NIST Traceable	10/05/2020, 10/12/2020	
NITRIC OXIDE	250.0 PPM	254.2 PPM	G1	+/- 0.5% NIST Traceable	10/05/2020, 10/12/2020	
PROPANE	250.0 PPM	252.8 PPM	G1	+/- 0.8% NIST Traceable	10/06/2020	
CARBON MONOXIDE	500.0 PPM	495.6 PPM	G1	+/- 0.6% NIST Traceable	10/07/2020	
CARBON DIOXIDE	5.000 %	4.843 %	G1	+/- 1.0% NIST Traceable	10/05/2020	
NITROGEN	Balance					

	CALIBRATION STANDARDS						
Туре	Lot ID	Cylinder No	Concentration	Uncertainty	Expiration Date		
NTRM	18060112	KAL004093	249.9 PPM NITRIC OXIDE/NITROGEN	+/- 0.4%	Nov 08, 2023		
PRM	12386	D685025	9.91 PPM NITROGEN DIOXIDE/AIR	+/- 2.0%	Feb 20, 2020		
GMIS	401438583103	EB0120479	3.882 PPM NITROGEN DIOXIDE/NITROGEN	+/- 2.1%	Feb 18, 2023		
NTRM	10060515	CC281302	495.3 PPM PROPANE/AIR	+/- 0.5%	Jan 06, 2022		
NTRM	13010109	KAL003925	495.4 PPM CARBON MONOXIDE/NITROGEN	+/- 0.6%	Jul 03, 2024		
NTRM	13060720	CC413719	16.939 % CARBON DIOXIDE/NITROGEN	+/- 0.6	May 14, 2025		
The SDM	DDM or DCM noted abo	un la antu la raforance t	n the CMIS used in the assay and not part of the analysis				

ANALYTICAL EQUIPMENT					
Instrument/Make/Model	Analytical Principle	Last Multipoint Calibration			
Nicolet 6700 AMP0900100	FTIR	Sep 10, 2020			
CO-1 SIEMENS ULTRAMAT 6E N1J5700	NDIR	Sep 23, 2020			
Nicolet 6700 AMP0900100	FTIR	Oct 09, 2020			
Nicolet 6700 AMP0900100	FTIR	Oct 09, 2020			
Nicolet 6700 AHR0801332	FTIR	Sep 10, 2020			

Triad Data Available Upon Request

PERMANENT NOTES: Mixture contains nominal 10ppm Sulfur Hexafluoride as a tracer component. Actual tested value included within the original Certificate of Analysis. Contact the Airgas laboratory if a reprint is required

NOTES:SF6 @ 10.15 PPM



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Page 1 of 54-401922301-1

9% O2/NO2



Airgas Specialty Gases Airgas USA, LLC 12722 S. Wentworth Ave. Chicago, IL 60628 Airgas.com

CERTIFICATE OF ANALYSIS Grade of Product: EPA Protocol

E03NI90E15W0003 CC511378 124 - Chicago (SAP) - IL B12020 NO2,O2,BALN Reference Number: 54-401922300-1
Cylinder Volume: 145.1 Cubic Feet
Cylinder Pressure: 2015 PSIG
660
Certification Date: 660
Oct 09, 2020 Part Number: Cylinder Number: Laboratory: PGVP Number: Gas Code:

S Code: NO2,O2,BALN

Expiration Date: Oct 09, 2023

Cortification performed in accordance with "EPA Traceability Protocol for Assay and Certification of Gaseous Calibration Standards (May 2012)" document EPA 600/R-12/S31, using the assay procedures listed. Analytical Methodology does not require correction for analytical interference. This cylinder has a total analytical uncertainty as stated below with a confidence level of 95%. There are no significant impurities which affect the use of this calibration mixture. All concentrations are on a mole/mole basis unless otherwise noted.

Do Not Us	e This Cylin	der below	100 psia i e	0.7 meganascal

ANALYTICAL RESULTS							
Component Requested Concentrati		Actual Concentration	Protocol Method	Total Relative Uncertainty	Assay Dates		
NITROGEN DIOXIDE	100.0 PPM	101.3 PPM	G1	+/- 1.2% NIST Traceable	10/02/2020, 10/09/2020		
OXYGEN	9.000 %	8.999 %	G1	+/- 0.7% NIST Traceable	10/02/2020		
NITROGEN	Balance						

		(CALIBRATION STANDARDS		
Type	Lot ID	Cylinder No	Concentration	Uncertainty	Expiration Date
GMIS	401424911103	CC506133	195.2 PPM NITROGEN DIOXIDE/NITROGEN	+/- 1.1%	Feb 10, 2023
PRM	12382	D685052	197.6 PPM NITROGEN DIOXIDE/AIR	+/- 1.0%	Sep 17, 2020
NTRM	98051116	SG9159580BAL	9.507 % OXYGEN/NITROGEN	+/- 0.7%	Oct 06, 2021
The SDM	DDM or DGM noted abo	ove is only in reference to th	e GMIS used in the assay and not part of the analysis		

ANALYTICAL EQUIPMENT					
Instrument/Make/Model	Analytical Principle	Last Multipoint Calibration			
MKS FTIR NO2 017707558	FTIR	Sep 17, 2020			
O2-1 HORIBA MPA-510 3VUYL9NR	Paramagnetic	Sep 10, 2020			

Triad Data Available Upon Request



Signature on file Approved for Release

Page 1 of 54-401922300-1

Ethylene Only



CERTIFICATE OF ANALYSIS Grade of Product: PRIMARY STANDARD

Part Number: Cylinder Number: Laboratory: Analysis Date: Lot Number: X02NI99P15ACVH8 CC420697 124 - Chicago (SAP) - IL Nov 06, 2020 54-401954197-1 Reference Number: Cylinder Volume: Cylinder Pressure: Valve Outlet: 54-401954197-1 144.4 CF 2015 PSIG 350

Expiration Date: Nov 06, 2023

Primary Standard Gas Mixtures are traceable to N.I.S.T. weights and/or N.I.S.T. Gas Mixture reference materials.

ANALYTICAL RESULTS

Component	Requested Concentration	Actual Concentration (Mole %)	Analytical Uncertainty
ETHYLENE	100.0 PPM	98.96 PPM	+/- 1%
NITROGEN	Balance		



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Page 1 of 54-401954197-1

Zero Gas/Nitrogen Bottle Certification



CERTIFICATE OF BATCH ANALYSIS **Grade of Product: BIP-BUILT IN PURIFIER**

NI BIP300 TW05-867349 Reference Number: 29-400672389-1 Cylinder Volume: 304.0 CF Cylinder Pressure: 2640 PSIG Valve Outlet: 580 Part Number: Cylinder Analyzed: MSO - Tulsa Fast Fill (SAP) - OK Feb 10, 2016 Laboratory: Analysis Date: Lot Number:

29-400672389-1

ANALYTICAL RESULTS

Component	Requested Purity	Certified Concentration
NITROGEN	99.999 %	99.999 %
OXYGEN	< 1 PPM	0.94 PPM
WATER	< 1 PPM	0.058 PPM
TOTAL HYDROCARBONS	< 0.1 PPM	0.1 PPM
CARBON DIOXIDE	< 0.5 PPM	0.235 PPM
CARBON MONOXIDE	< 0.5 PPM	0.235 PPM

Permanent Notes: This cert includes values from the "fill" side and is not representative of the "use" side purity. Contact an Airgas Sales Representative for this information.

4263617Y, TW04671107, TW05-831574, TW05-865966, TW05-867349, TW05-867538, TW05-867578, TW05-881687, TW05-881820, TW05-920689, TW05-920760, TW05848694, TW05867441, TW05897265, TW05897512, TW05920678, TW05920686, TW05920695,

Impurities verified against analytical standards traceable to NIST by weight and/or analysis.

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21% 02



CERTIFICATE OF ANALYSIS Grade of Product: EPA Protocol

E02NI79E15A00B1 CC317205 124 - Pasadena (SG06) - TX A32019 O2,BALN Reference Number: 163-401680474-1 Cylinder Volume: 146.2 CF Cylinder Pressure: 2015 PSIG Part Number: Cylinder Number: Laboratory: Valve Outlet: Certification Date: PGVP Number: 590 Dec 16, 2019 Gas Code:

Is Code: U2,BALN

Expiration Date: Dec 16, 2027

Expiration Date: Dec 16, 2027

Certification performed in accordance with "EPA Traceability Protocol for Assay and Certification of Gaseous Calibration Standards (May 2012)" document EPA 600R-12/531, using the assay procedures listed. Analytical Methodology does not require correction for analytical interference. This cylinder has a total analytical uncertainty as stated below with a confidence level of 95%. There are no significant impurities which affect the use of this calibration mixture. All concentrations are on a molecular process of the proces

	ANALYTICAL RESULTS							
Component	Requeste Concentr		Actual Concentration	Protocol Method	Total Relative Uncertainty	Assay Dates		
OXYGEN NITROGEN	21.00 % Balance	2	21.06 %	G1	+/- 0.7% NIST Traceable	12/16/2019		
Туре	CALIBRATION STANDARDS Type Lot ID Cylinder No Concentration Uncertainty Expiration Date							
NTRM	08010502	K010502	23.20 % O	KYGEN/NITROGEN	+/-0.4%	Jun 01, 2024		
ANALYTICAL EQUIPMENT								
Instrument/Make/Model Analytical Principle Last Multipoint Calibration								
O2-SIEMENS	O2-SIEMENS OXYMAT 6 DD550 PARAMAGNETIC Dec 09, 2019							

Triad Data Available Upon Request



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Page 1 of 163-401680474-1

Tri Probe Certification



Great Plains Analytical Services

303 W 3rd St

Elk City, OK, 73644

(580)225-0403 Fax: (580)225-2612

CERTIFICATE OF ANALYSIS

Grade of Product: CERTIFIED STANDARD-PROBE

Part Number: 16

A-0016

Reference Number:

Laboratory: GREATPLAINS

Stack Diameter: 16

16"

Analysis Date:

Cylinder Number:

Flow Rate:

Rate: 3L/min

Number of

Points:

LOT Number: 0001

Air Liquide ALM060675

Jan. 18, 2018

Product performance verified by direct comparison to calibration standards traceable to N.I.S.T. weights and/or N.I.S.T. Gas Mixture reference materials.

*The probe listed on this form meets the multipoint traverse requirement of EPA Method 7e, section 8.4 as shown in the accompanying data. Method 7e, section 8.4 states that the multipoint traverse requirement can be satisfied by sampling via "a multi-hole probe designed to sample at the prescribed points with a flow within 10 percent of mean flow rate".

ANALYTICAL RESULTS

Component	Cylinder Concentration	Concentration Port A (Difference from Mean)	Concentration Port B (Difference from Mean)	Concentration Port C (Difference from Mean)	Mean Probe Port Sampled Concentration	Maximum Error
SF6 – SULFUR HEXAFLUORIDE	10.31 PPM	3.42 (0.09%)	3.37 (1.2%)	3.45 (1.12%)	3.41	1.2%
C2H40 – ACETALDEHYDE	103.84 PPM	34.02 (0.4%)	33.65 (0.71%)	33.99 (0.32%)	33.89	0.71%

*Concentration error in this certification is defined as the percent difference between the concentration of gas sampled at a particular port and the mean concentration sampled at all ports on probe.

Notes:

Jan 18, 2018

Approved for Release

Date